



# Visual and Raman spectroscopic observations using fused silica capillary reactor technique



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## ★ Fused Silica Capillary Reactor (FSCR)

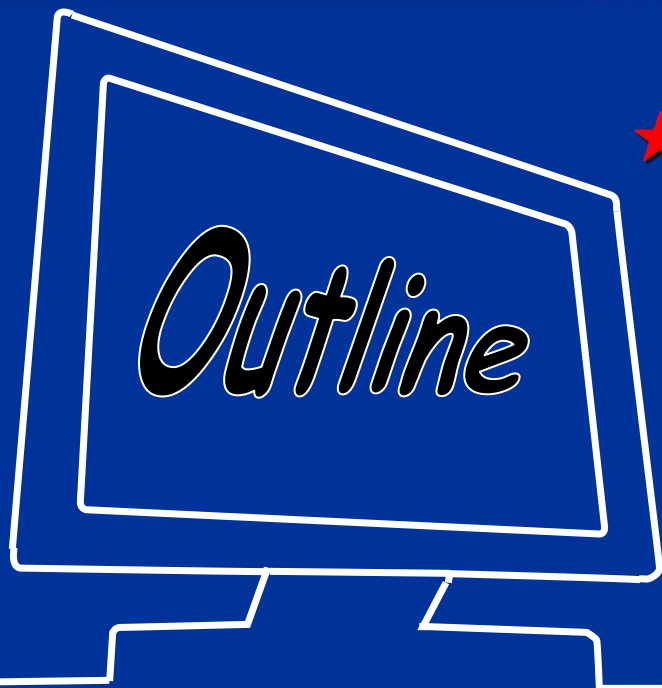
★ Measurement of solubilities in FSCR

★ Supercritical water oxidation in FSCR

★ Depolymerization of polyester

★ Determining the volume expansion

★ Summary






**FSCR?**

**What is**

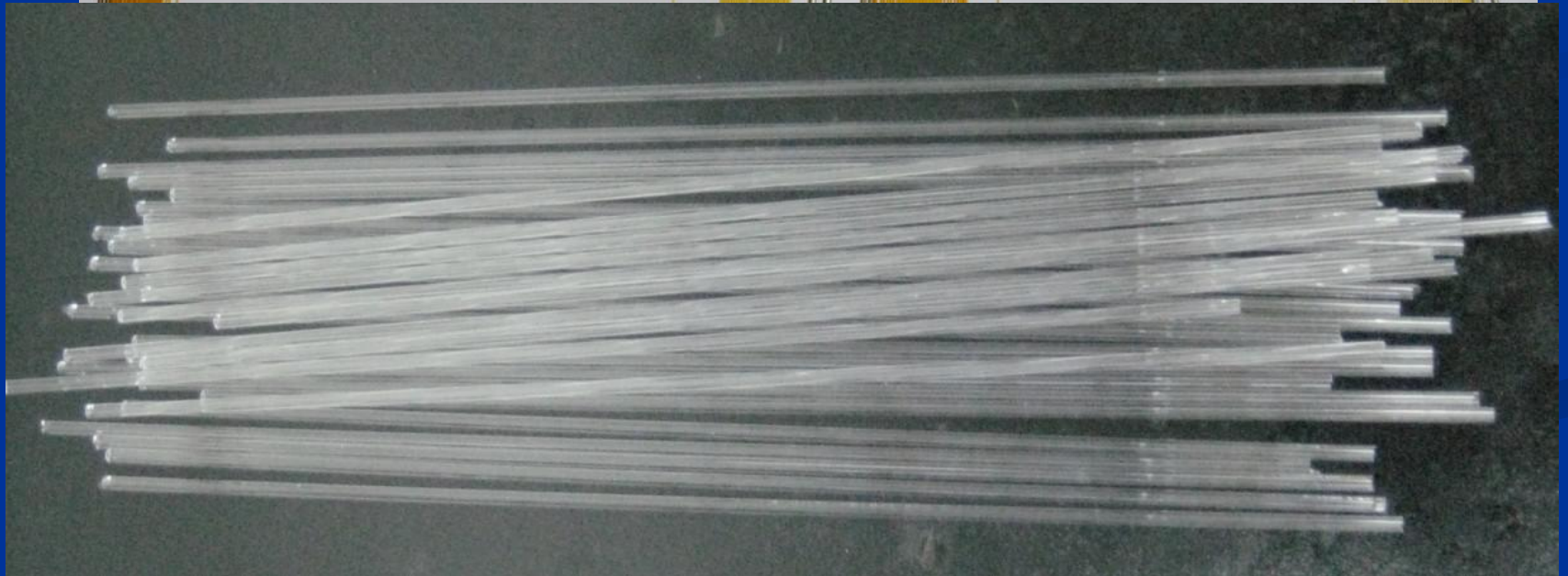
**Fused Silica  
Capillary  
Reactor?**

# Fused Silica Capillary Reactor (FSCR)

- 
- Raw materials
  - Manufacturing process
  - Heating-cooling stage & Raman spectroscopy
  - FSCR sample

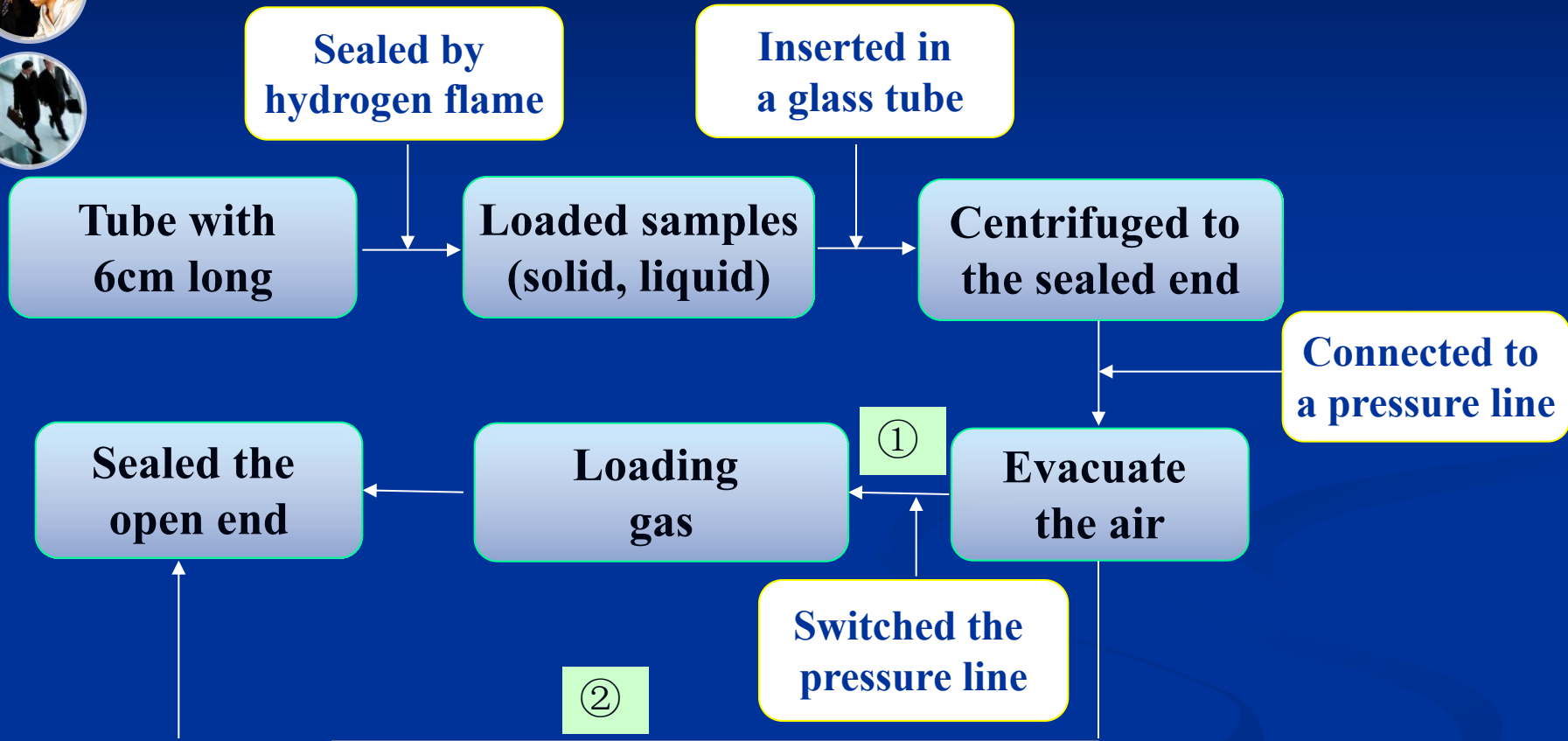


# 1.1 Raw materials



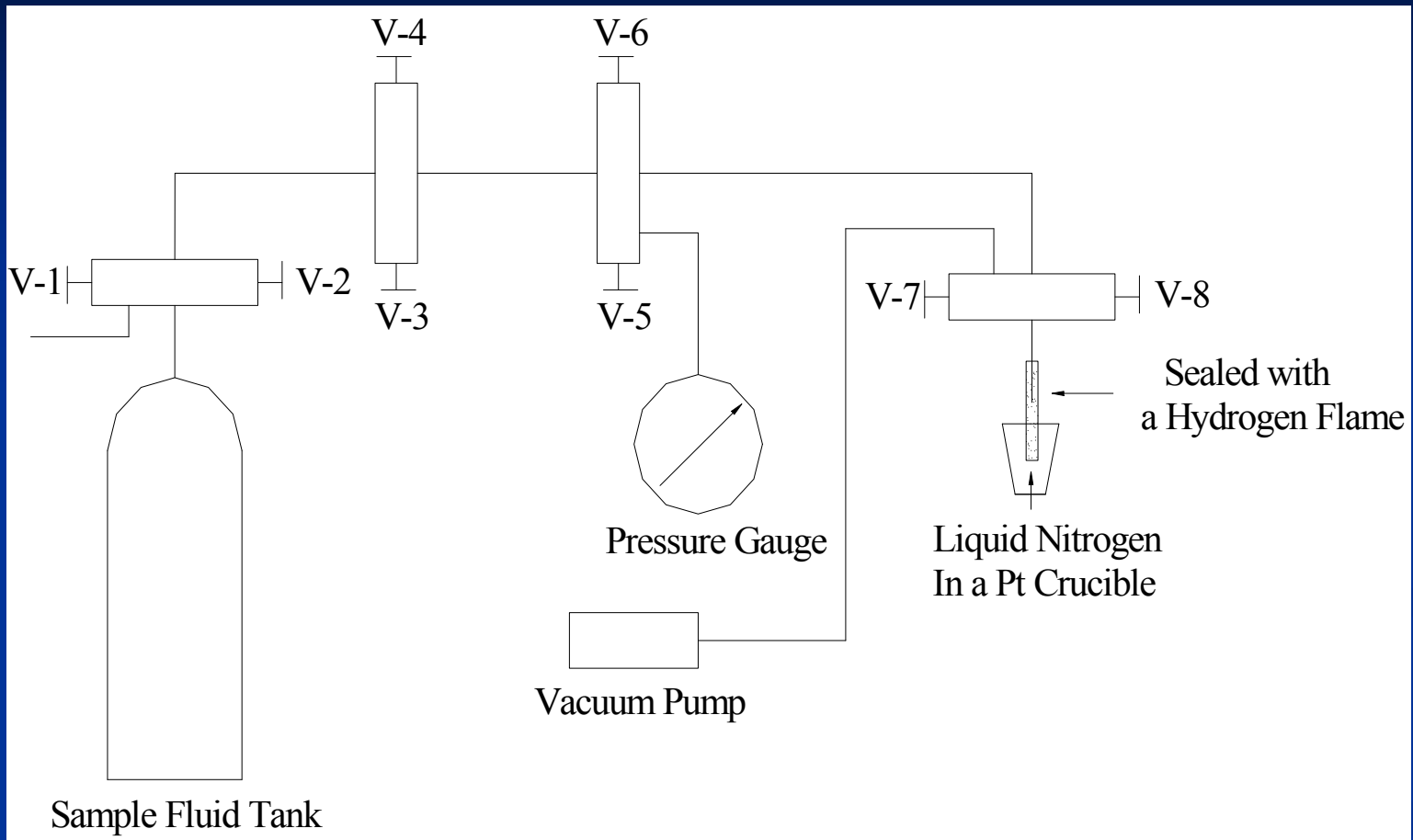


# 1.2 Manufacturing process



## Schematic of Synthesizing of FSCR

Fused silica capillary reactor (FSCR) was constructed from capillary tube, which has a shape of round cross-section (OD 0.66 mm /ID 0.30 mm).



**Schematic Diagram of the Vacuum  
and Sample Loading System**





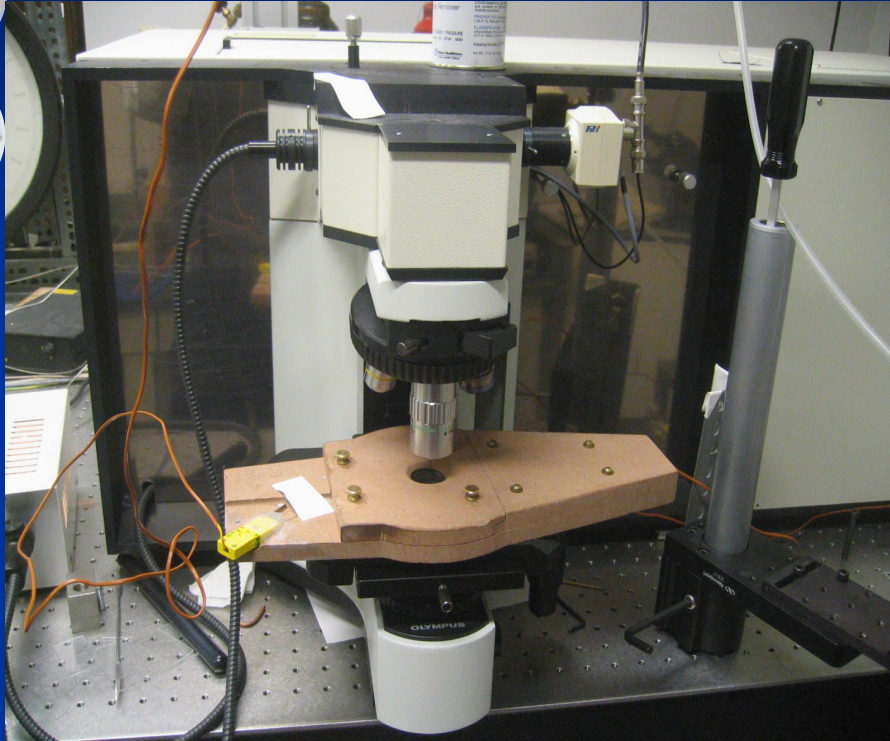
# 1.2 Manufacturing process



Photogram of the Vacuum and Sample Loading System



# 1.3 Heating–cooling stage

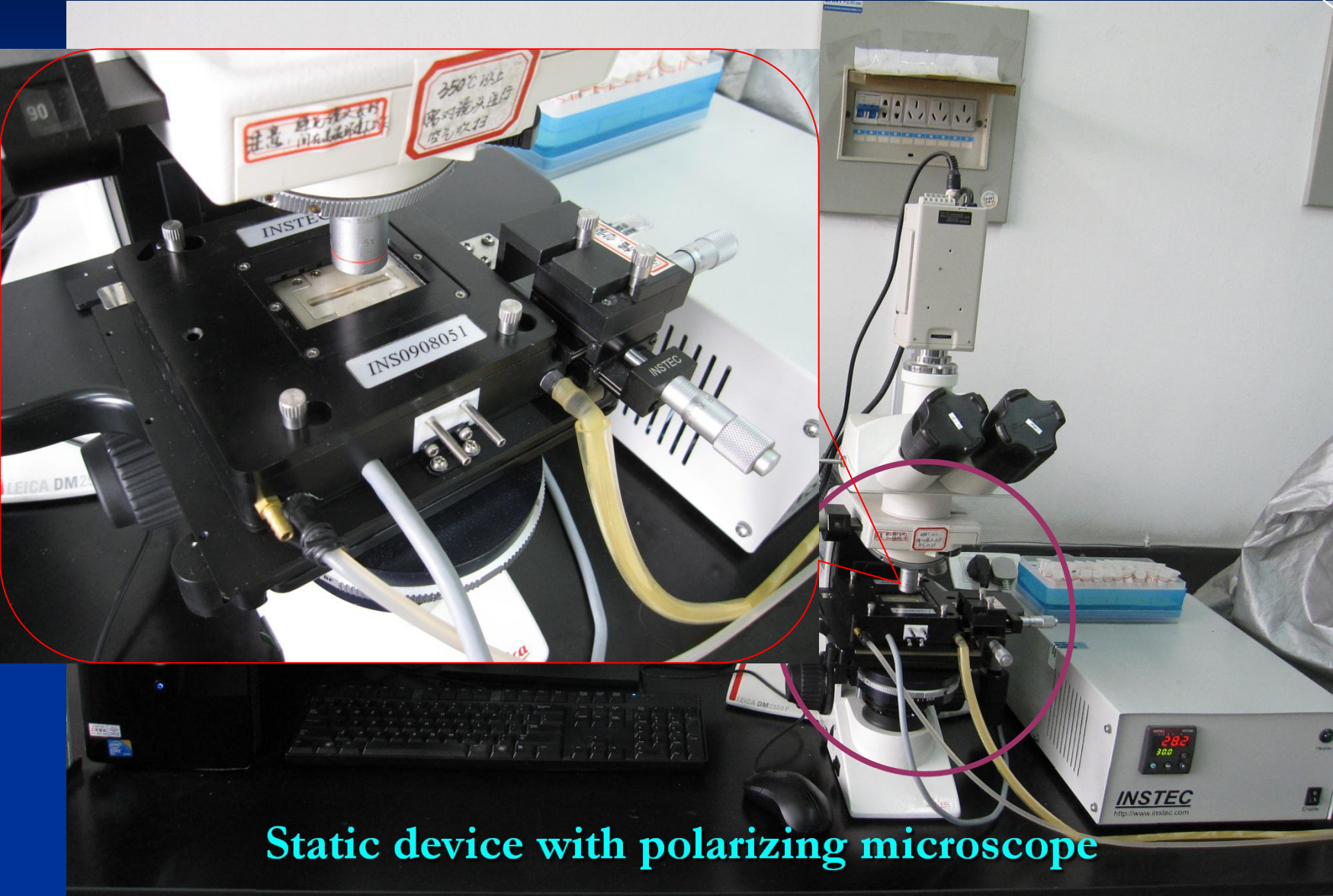


Heating–cooling stage of USGS  
Raman Spectroscopy

The FSCR prepared was inserted into the sample chamber of the USGS-type heating-cooling stage, where the temperature could be controlled and maintained by continuous flow of heated air, and read by a K-type thermocouple with an accuracy of  $\pm 0.2\text{K}$ .



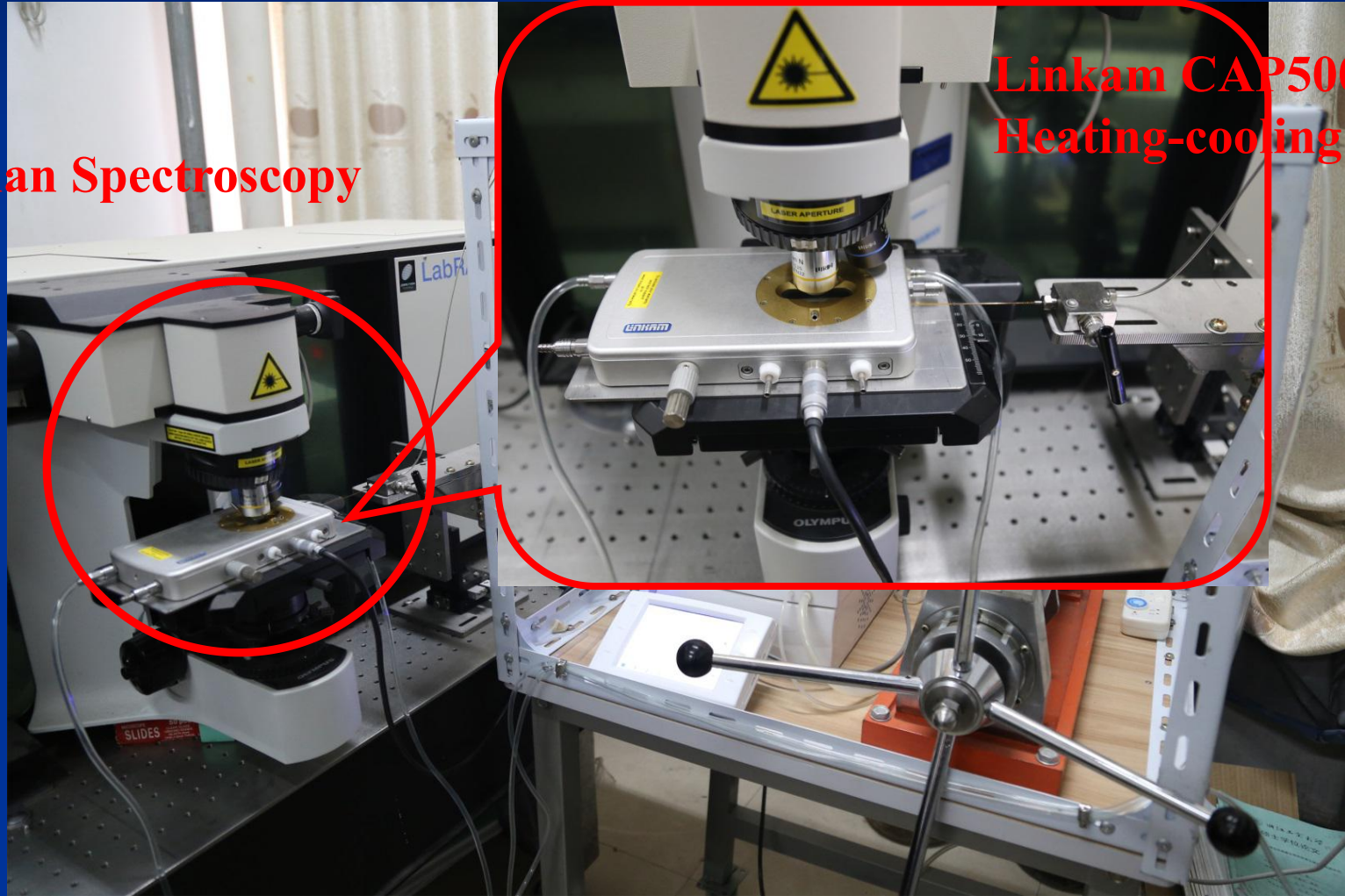
# INSTECH heating-cooling stage



Static device with polarizing microscope

# Linkam heating-cooling stage

Raman Spectroscopy



Linkam CAP500  
Heating-cooling stage



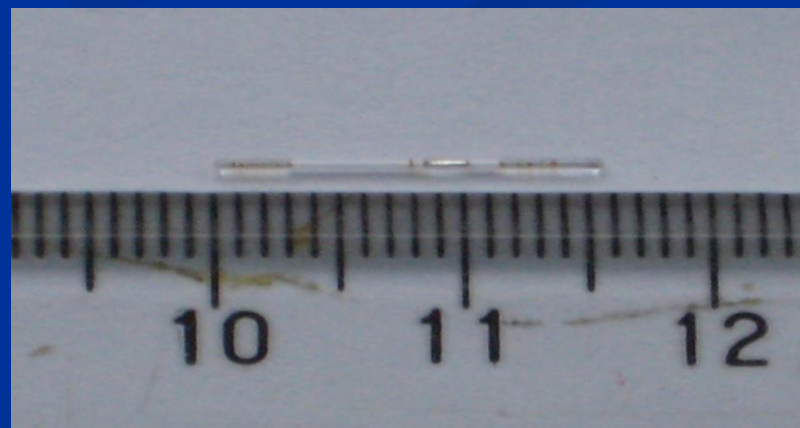
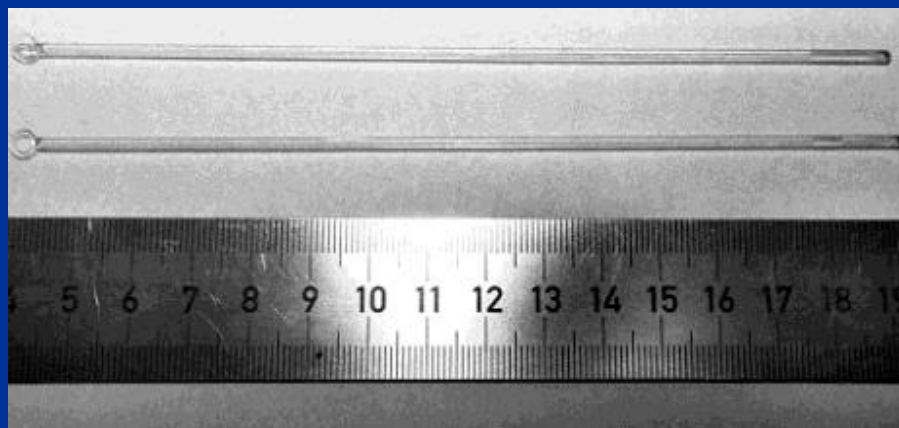
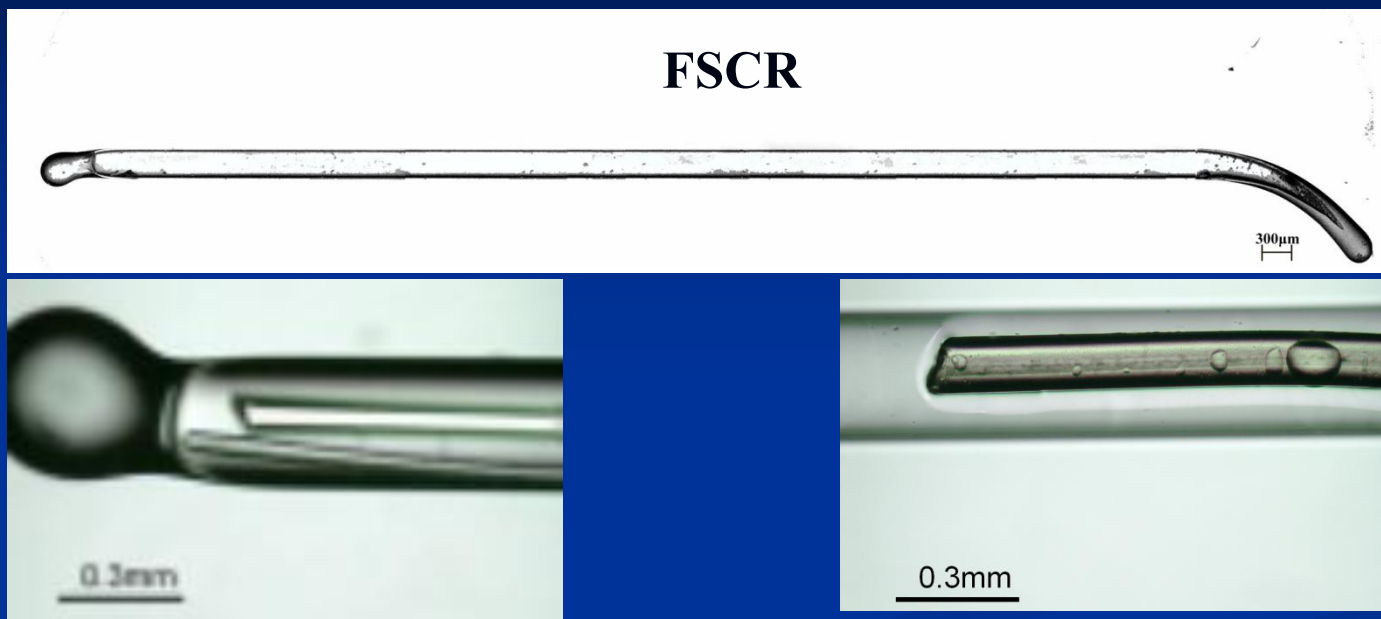
# Raman Spectroscopy





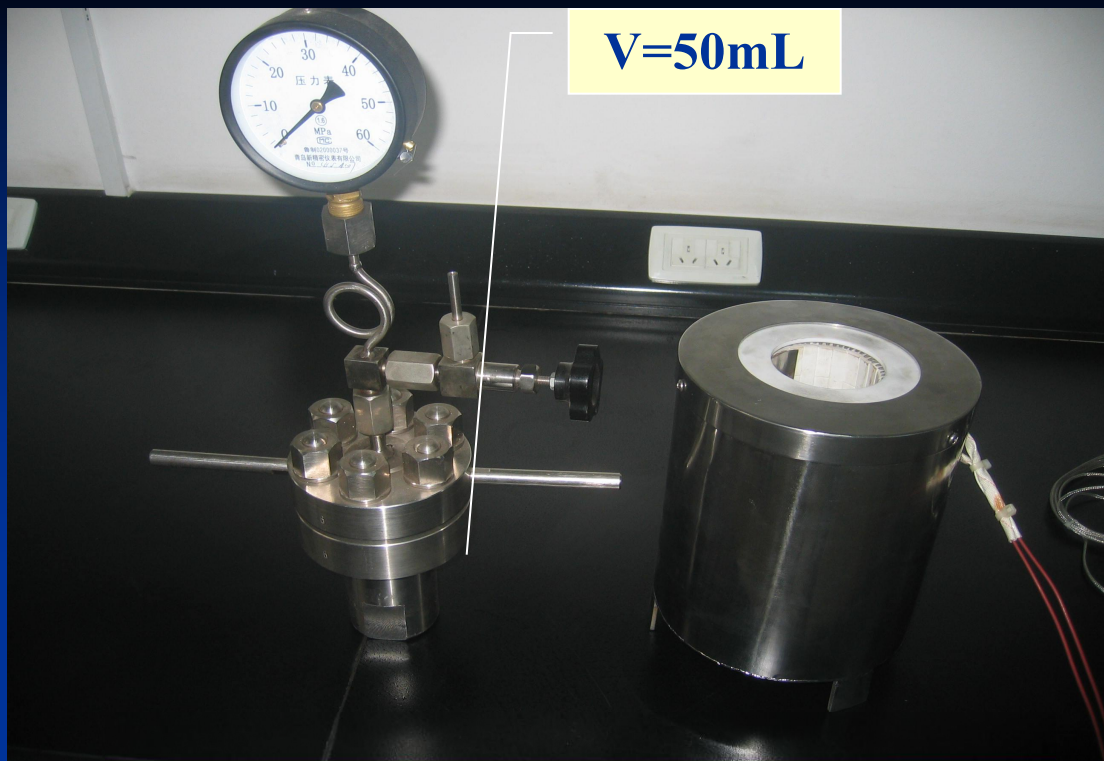


# 1.4 FSCR sample



Photograph of the capillaries  
(0.3mm ID, 0.66mm OD, and ~25mm long)

➤ *Green Chemistry*, 2009, 11: 1105-1107.



Minisize high-pressure reactor



$V=0.001\sim 0.005\text{mL}$

Fused silica capillary reactor (FSCR)



$V=500\sim 5000\text{mL}$

stainless steel autoclave

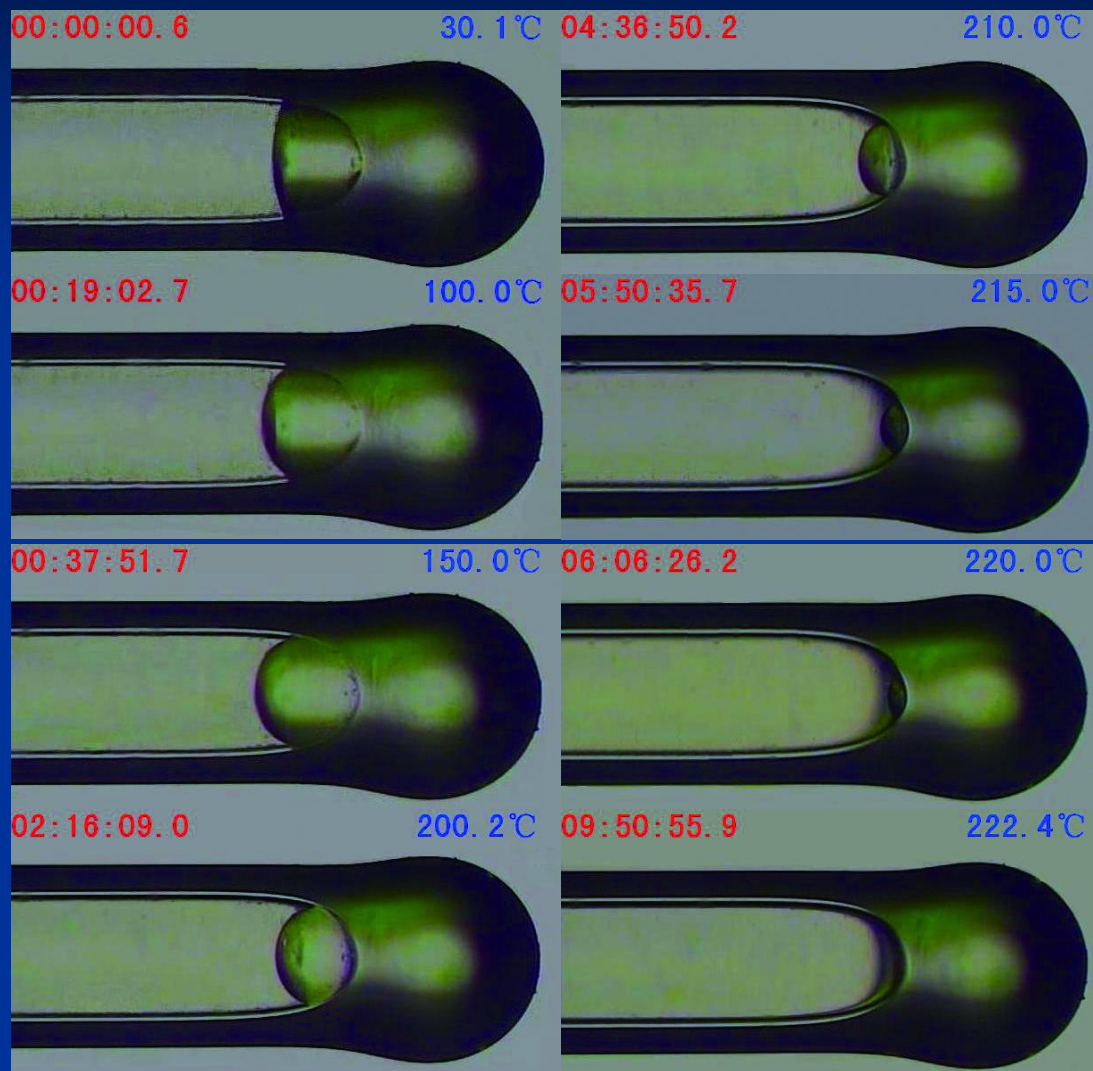
# Measurement of solubilities in FSCR



- Solubility of chlorobenzene in hot compressed water (HCW)
- Solubility of 2,4-dichlorotoluene in HCW by in situ Raman spectroscopy
- Solubility of ethanol in SC-CO<sub>2</sub> with FSCR



## 2.1 Solubility of chlorobenzene in HCW with FSCR

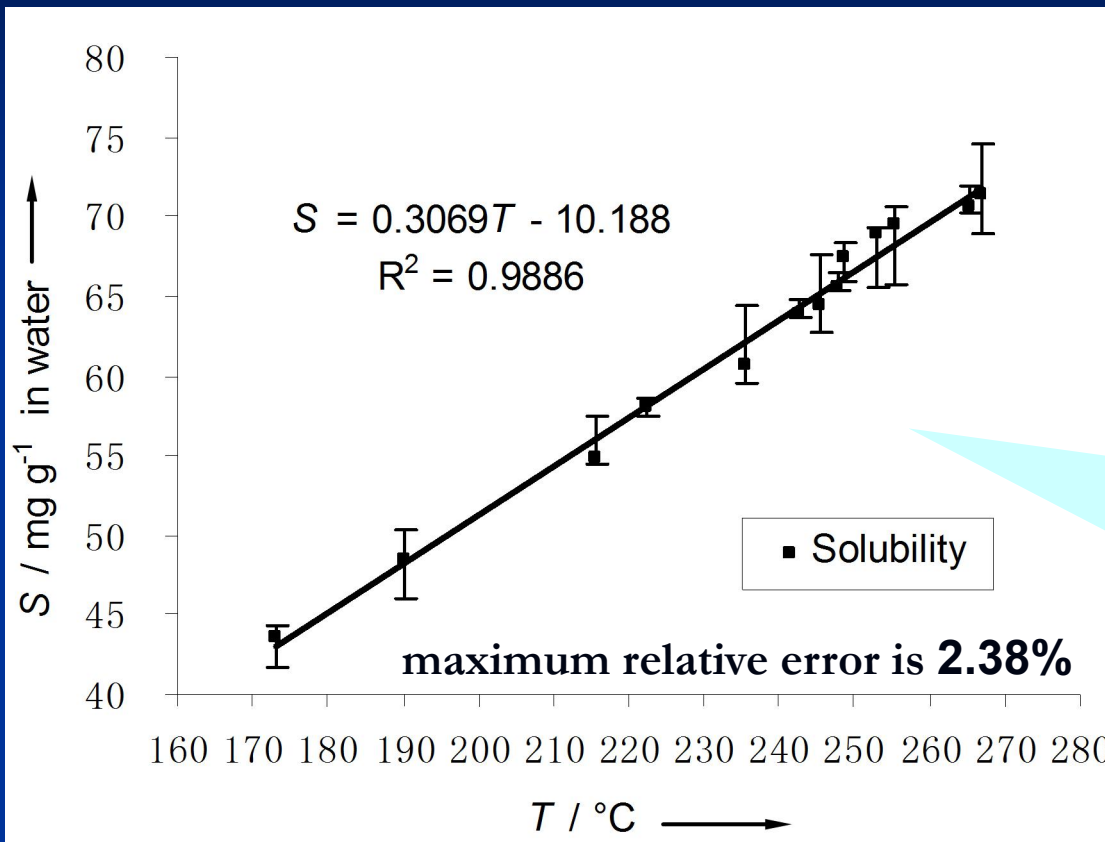


FSCR was heated to the preset temperature and allowed the sample to equilibrate for a period between 8 and 10h in the presence of a vapor phase. For example, the images of a sample containing 58.0 mg of  $C_6H_5Cl$ /g of  $H_2O$ , taken during heating from 30.1 to 222.4°C, they show the gradual dissolution of  $C_6H_5Cl$  during heating and its total disappearance at 222.4 °C.

Dissolution of chlorobenzene in water during heating.

The  $C_6H_5Cl$  is shown at the right end of the FSCR. The FSCR is under the microscope

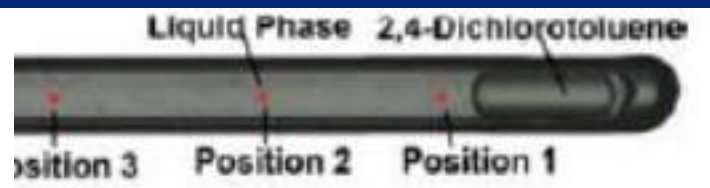
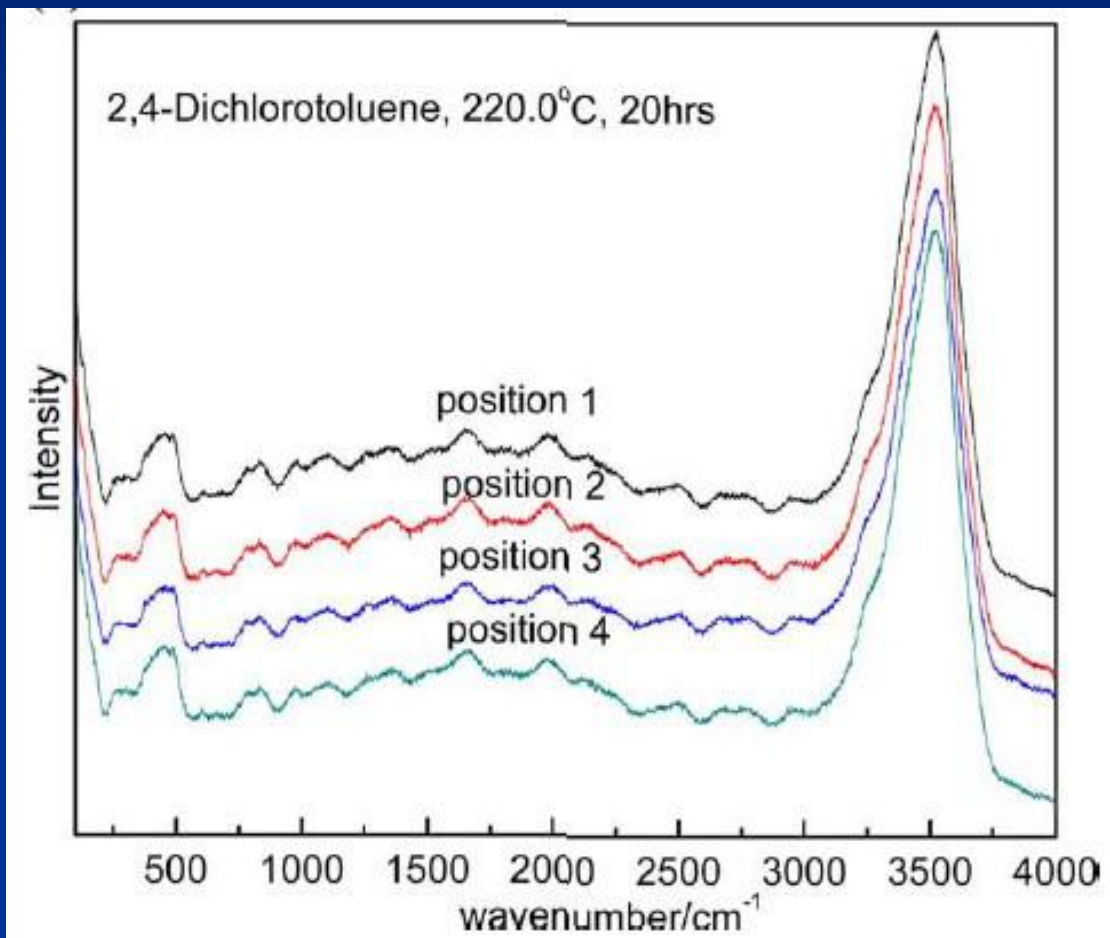
# Temperature range (173.3 ~ 266.9 °C)



The results indicate the solubility of  $C_6H_5Cl$  increases with increasing temperature, and can be represented by the linear equation

Solubility of  $C_6H_5Cl$  in pure water at temperatures between 173.3 and 266.9 °C  
■, experimental data; —, least-squares fit of the data

## 2.2 Solubility of 2,4-Dichlorotoluene in HCW with FSCR by in Situ Raman spectroscopy

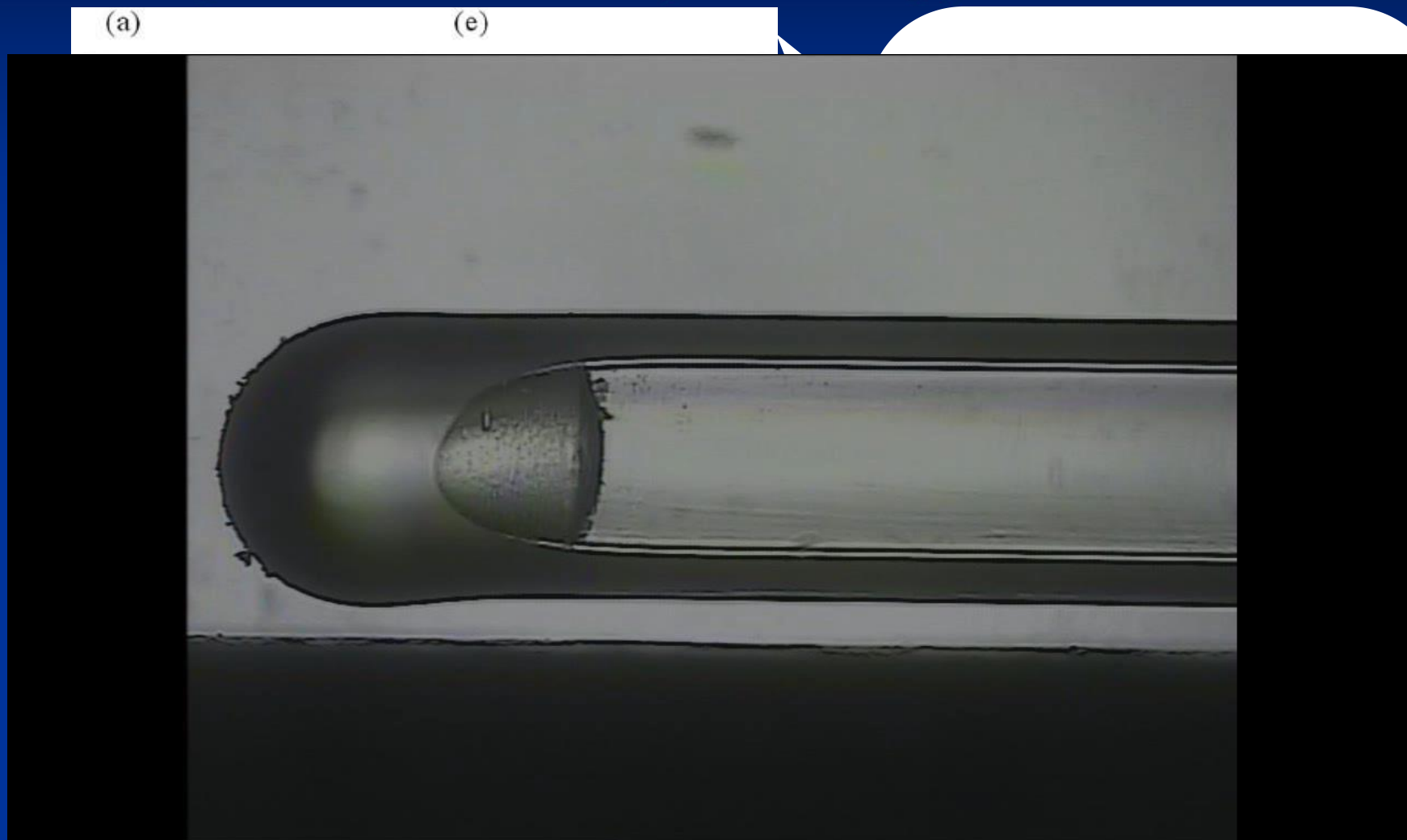


2,4-dichlorotoluene, liquid phase,  
spots for F

The Figure shows that the Raman spectra of 2,4-dichlorotoluene had bands with the same relative intensities at 457.04 cm<sup>-1</sup> and 828.54 cm<sup>-1</sup>. It can be concluded that the solute diffused uniformly and the system reached phase equilibrium within a certain time, proving that the apparatus is viable.

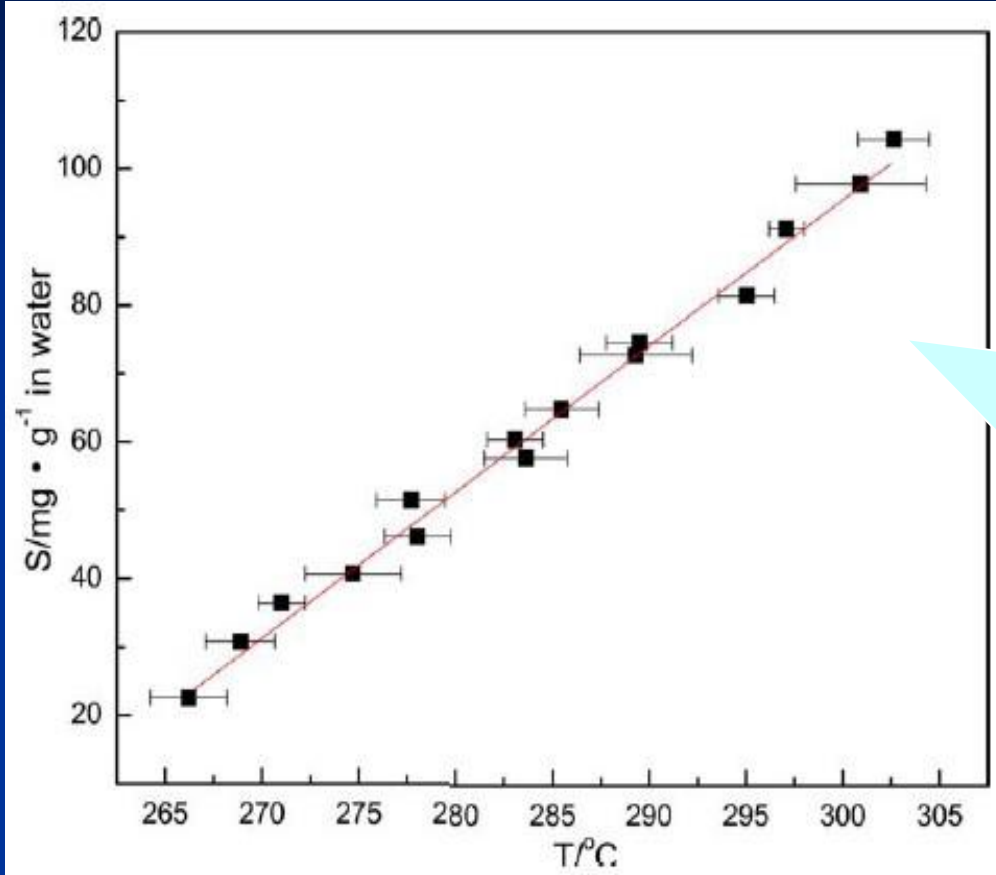
An image of Raman spectra of liquid phase in the FSCR at four spots, at 220.0C, 20 h.

## 2.2 Solubility of 2,4-dichlorotoluene in HCW with FSCR by in Situ Raman spectroscopy



**Dissolution of 2,4-dichlorotoluene in HCW during heating process.  
2,4-Dichlorotoluene is at the left of the FSCR.**





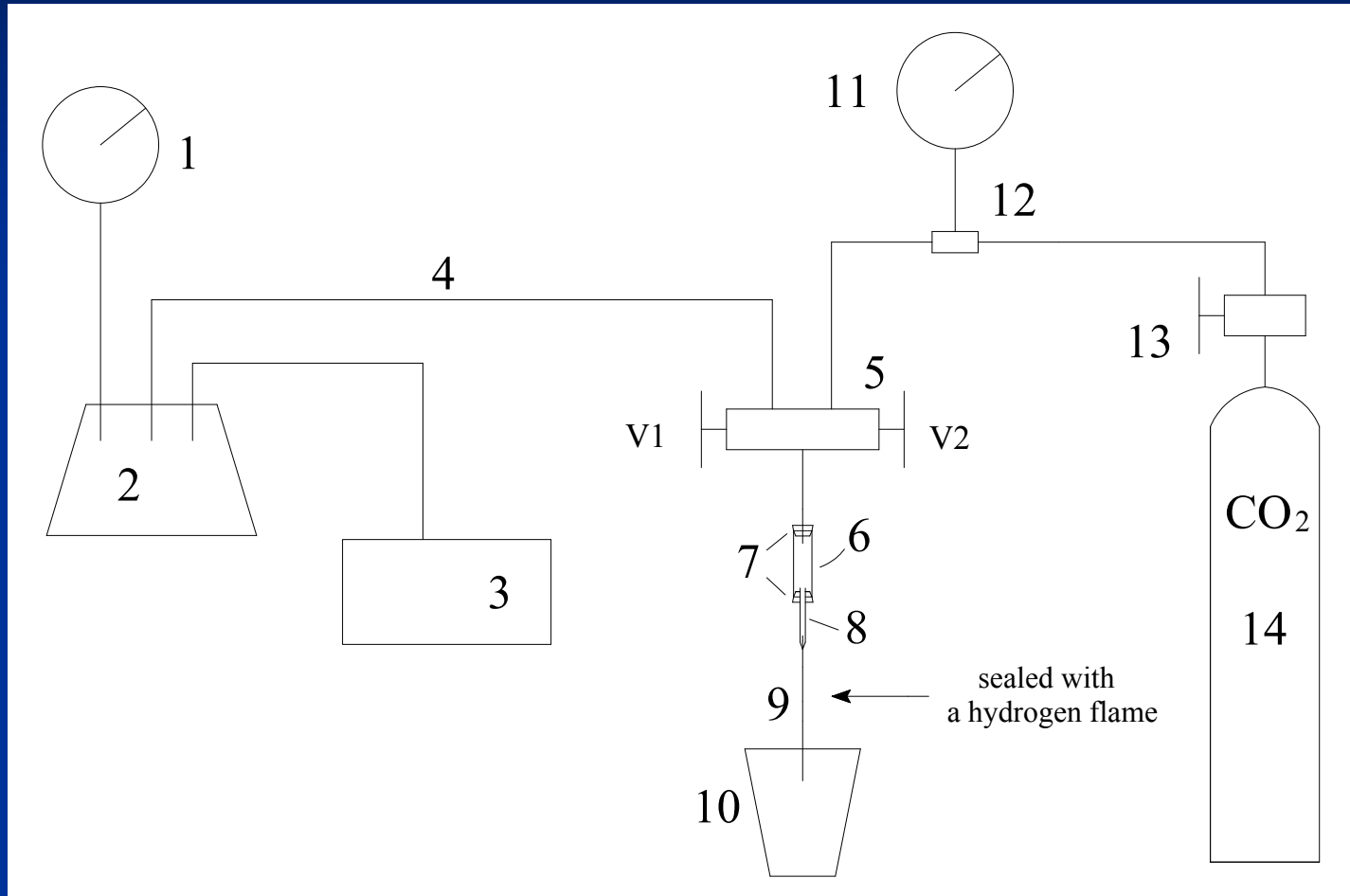
The results indicate that the solubility of 2,4-dichlorotoluene increased from 22.6 to 104.2 mg/(gH<sub>2</sub>O) when the temperature rose from 266.3 to 302.4°C

Solubility of 2,4-dichlorotoluene in water at temperatures between 266.3 and 302.4°C: (■) experimental data; (--) least-squares fit of the data.

*AICHE Journal, 2013, 59 (8):2721-2725.*

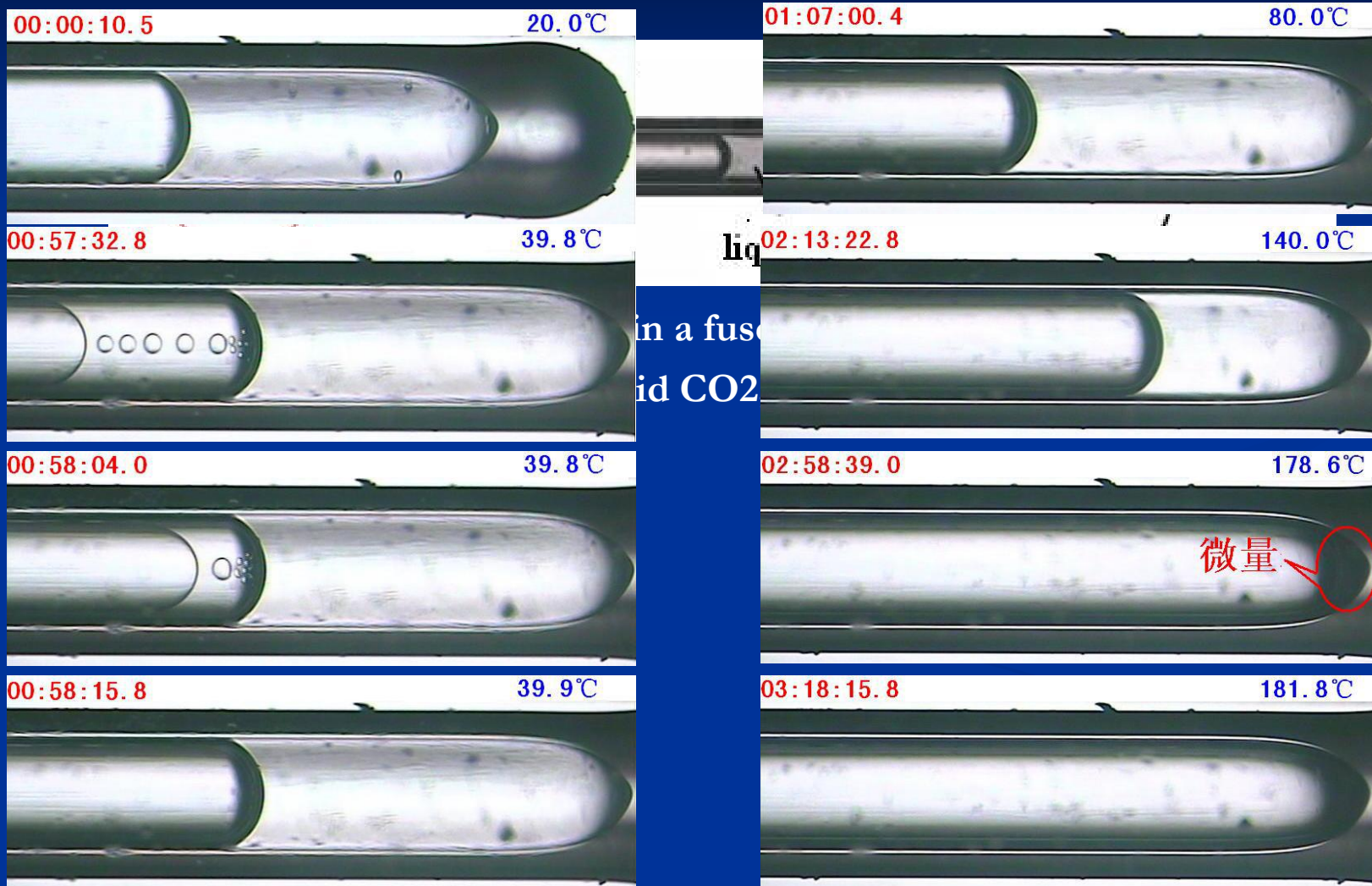


## 2.3 Solubility of ethanol in SC-CO<sub>2</sub> with FSCR



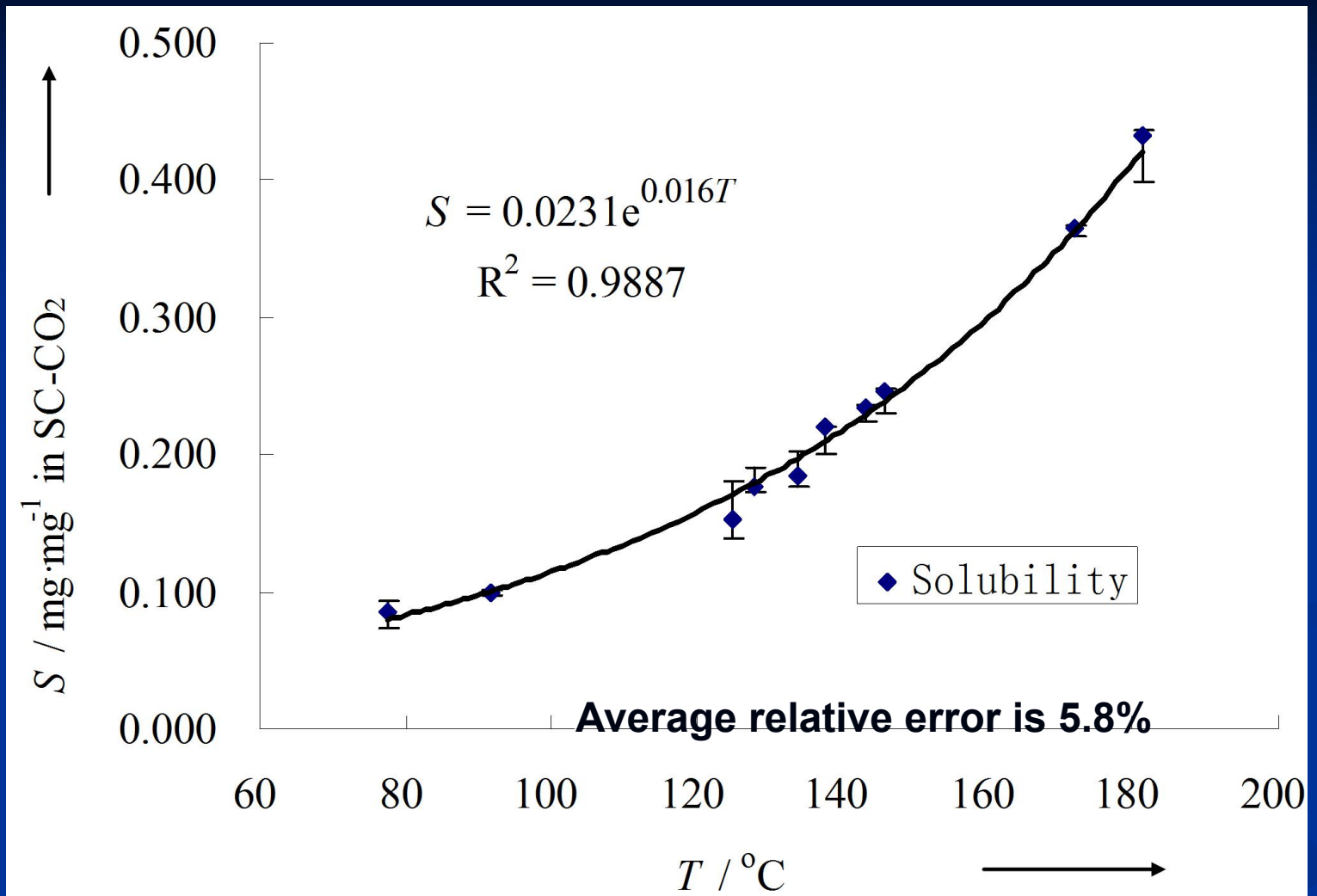
Schematic diagram of the experimental flow to determine the solubility of ethanol in SC-CO<sub>2</sub>

## 2.3 Solubility of ethanol in SC-CO<sub>2</sub> with FSCR



Dissolution of ethanol in supercritical CO<sub>2</sub> during heating.

The ethanol is shown at the right end of the FSCR, and the FSCR is under the microscope.



Solubility of ethanol in SC-CO<sub>2</sub> at temperatures between 87.5 and 183.8°C  
■, experimental data; —, least-squares fit of the data.



# Supercritical water oxidation in FSCR

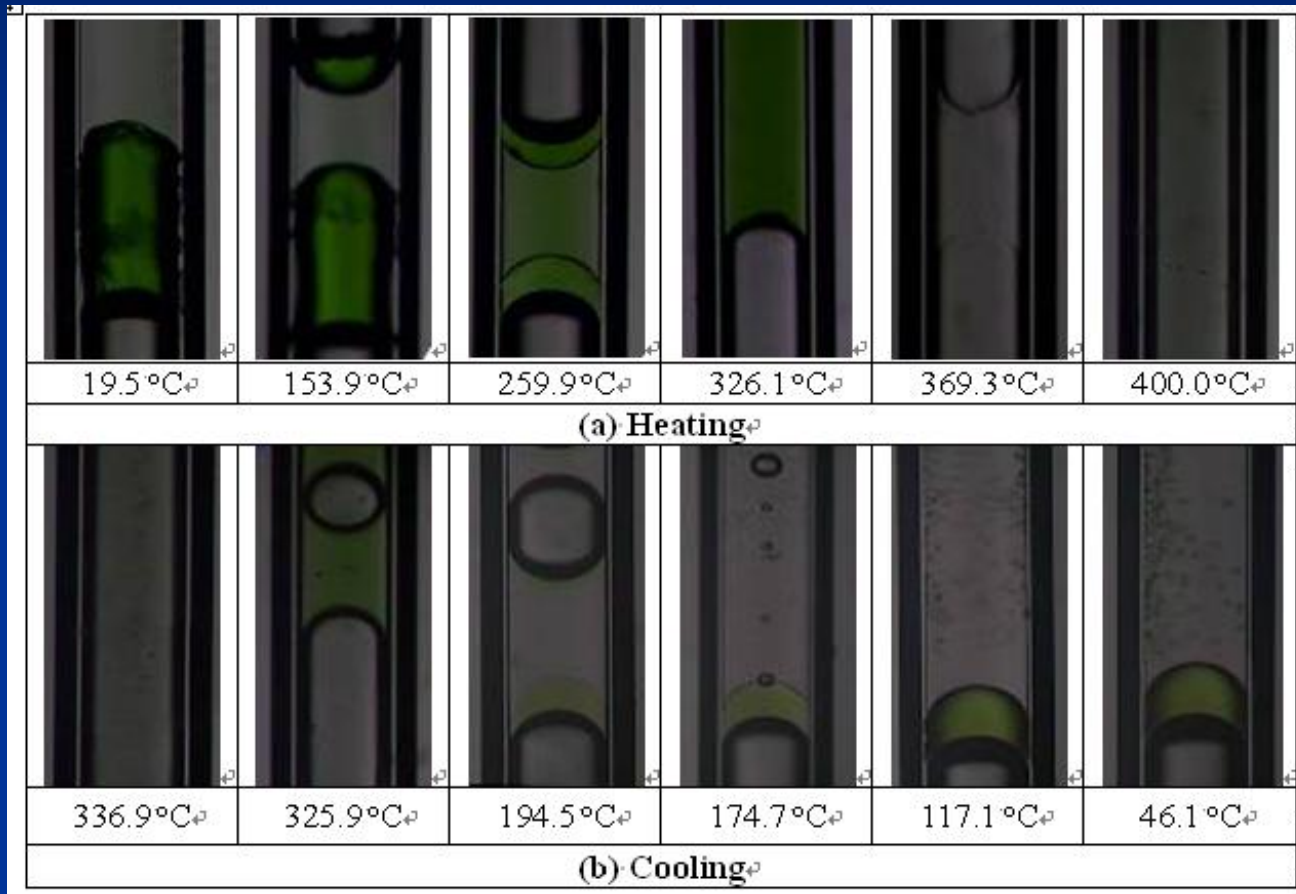
● Supercritical water oxidation of **chlorobenzene (CB)**

● Hydrolysis of  $\text{CCl}_4$  in HCW

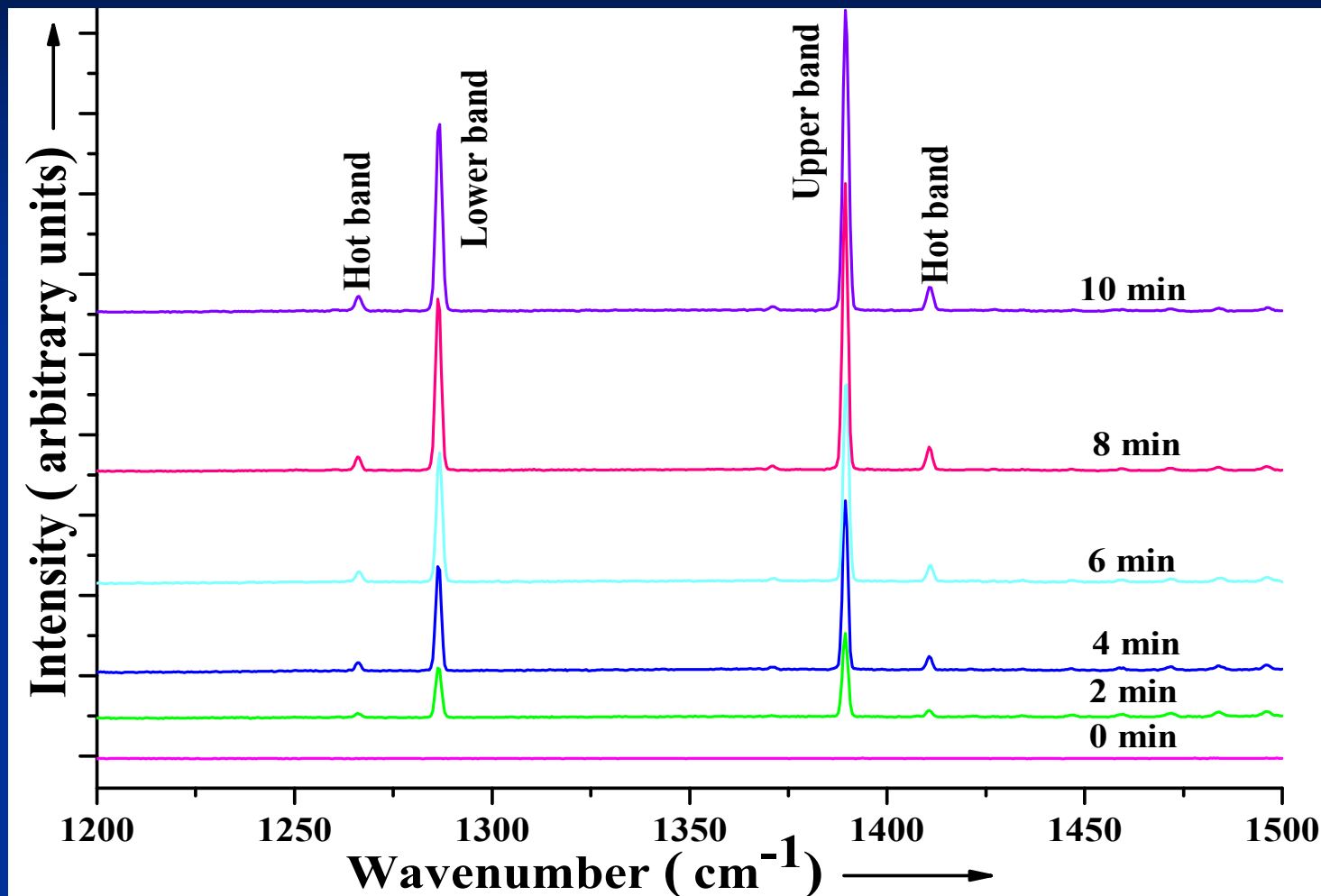
● Decomposition of 1,1,1-trichloroethane (TAC) in HCW



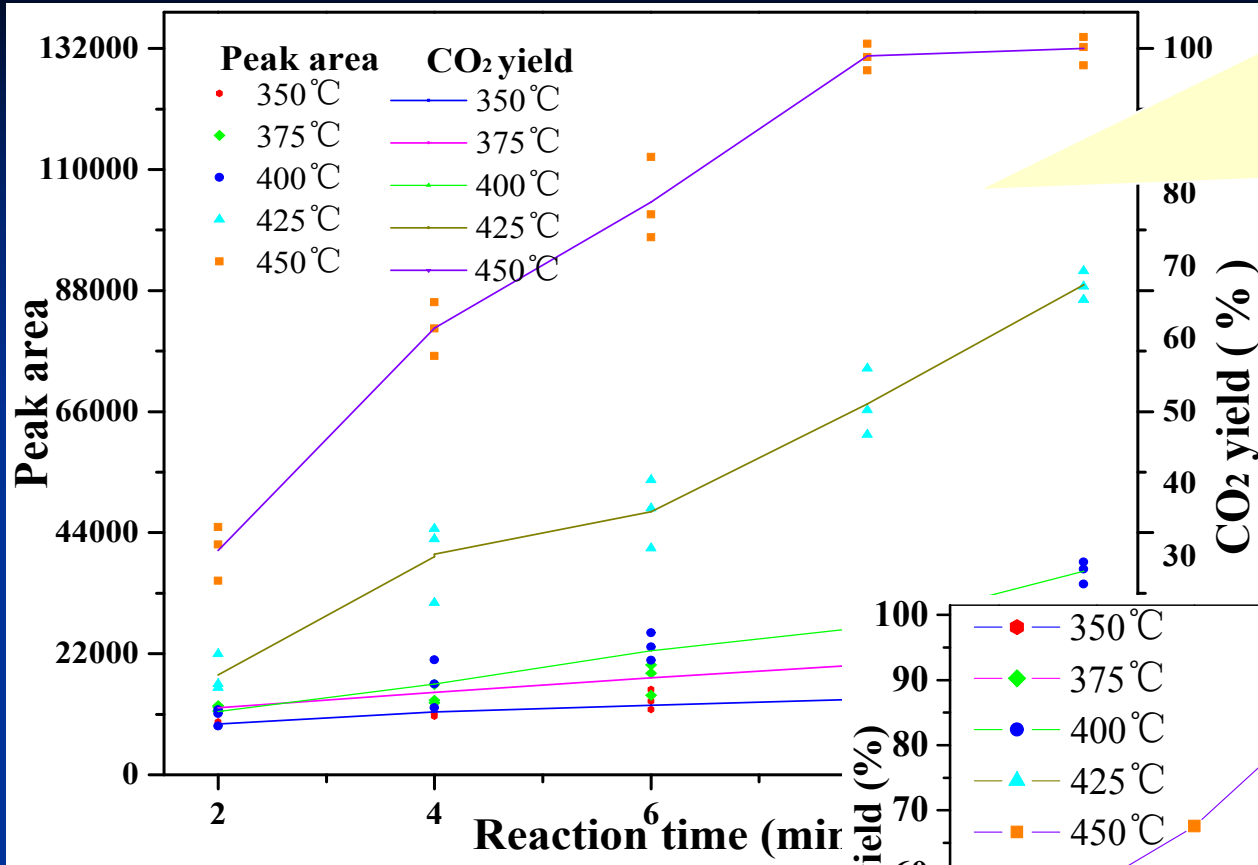
# 3.1 Phase-behavior changes of CB in the FSCR



Photomicrographs of chlorobenzene in hydrogen peroxide (30 wt%) in a fused-silica capillary reactor during heating process (a), and cooling process (b).

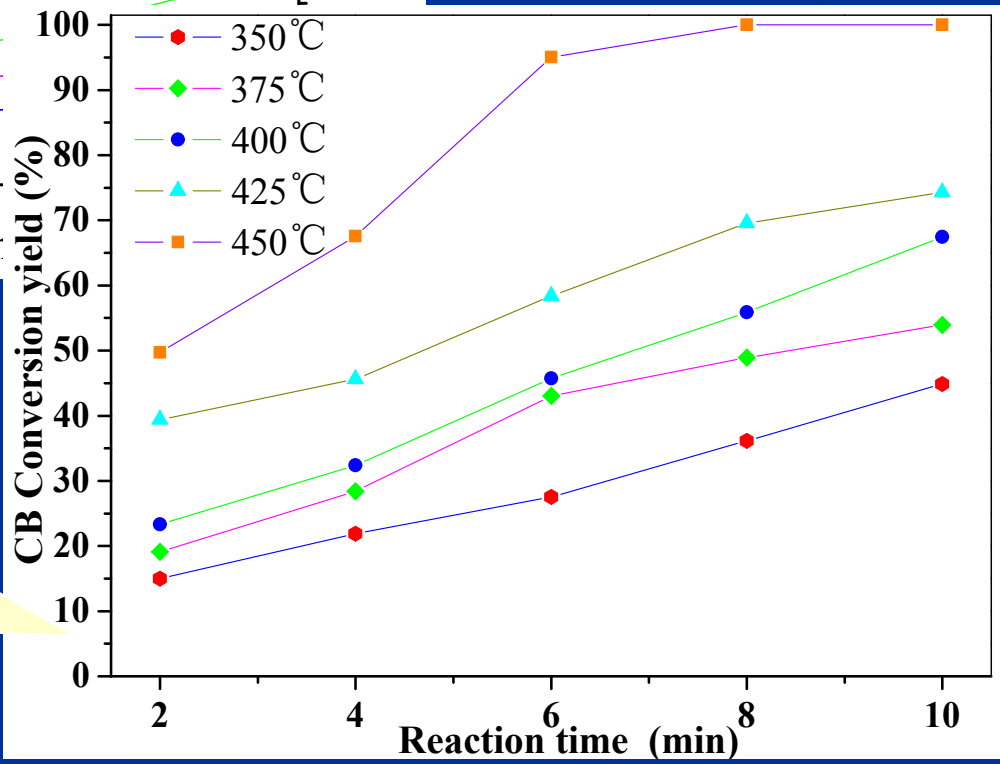


**Raman spectra of CO<sub>2</sub> produced by oxidation of CB in supercritical water with 150% stoichiometric amounts of oxidizer at 450 °C at different reaction times.**



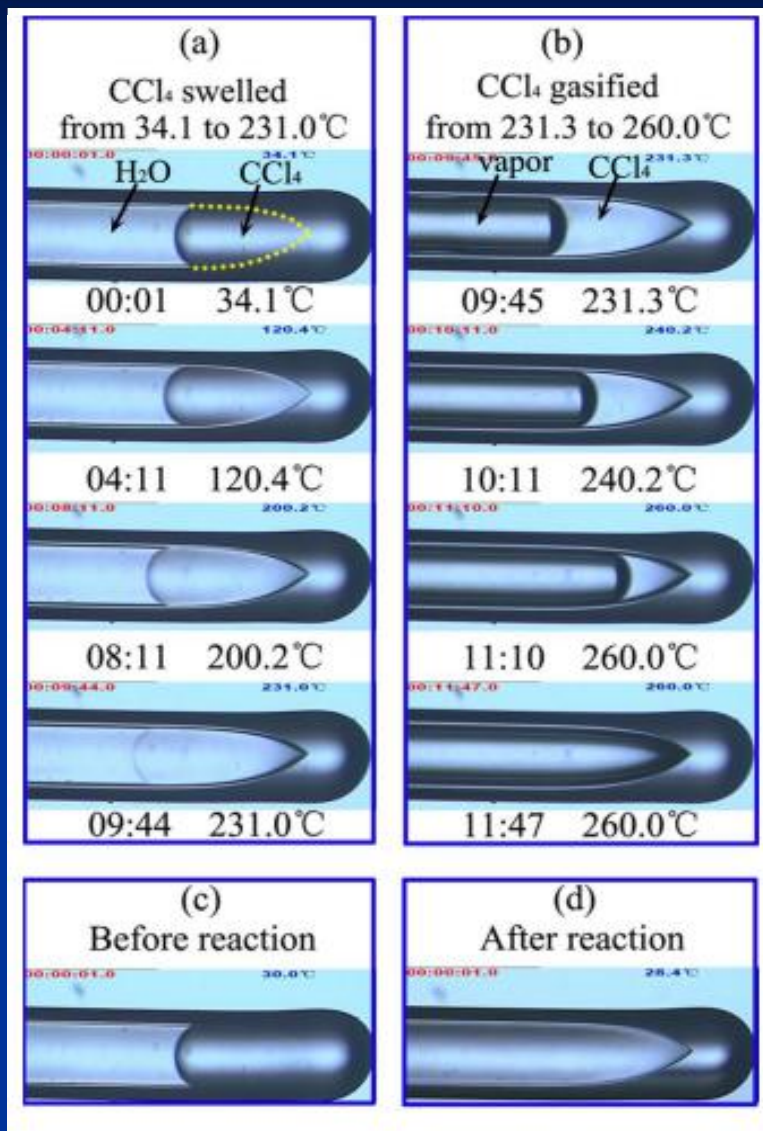
Raman peak area of CO<sub>2</sub> (scattered symbols) and CO<sub>2</sub> yield (lines) vs reaction time with 150% stoichiometric amount of oxidizer at different temperatures.

Effects of reaction time on CB conversion yield with 150% stoichiometric amount of oxidizer at different temperatures.





# 3.2 Hydrolysis of $\text{CCl}_4$ in FSCR

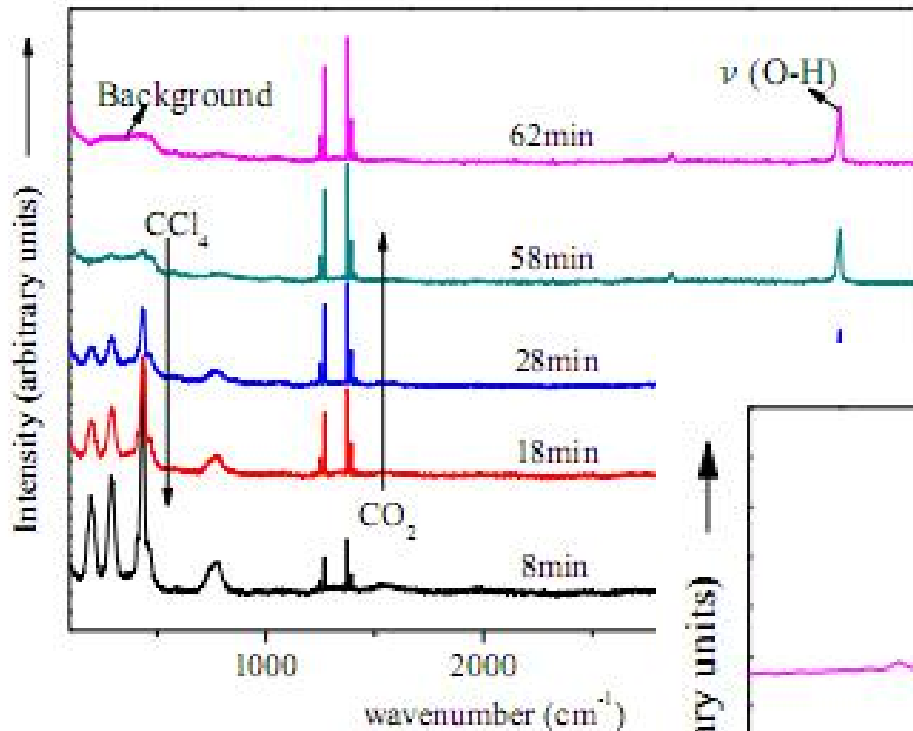


Photomicrographs of  $\text{CCl}_4$  with water in FSCR during the heating process: (a)  $\text{CCl}_4$  swells up between 34.1 and 231.0°C and gasifies (b) between 231.3 and 260.0°C. (c) Photomicrographs before and (d) after reaction taken at room temperature.

➤ In Situ Raman Spectroscopic Study of Hydrolysis of Carbon Tetrachloride in Hot Compressed Water in a Fused Silica Capillary Reactor

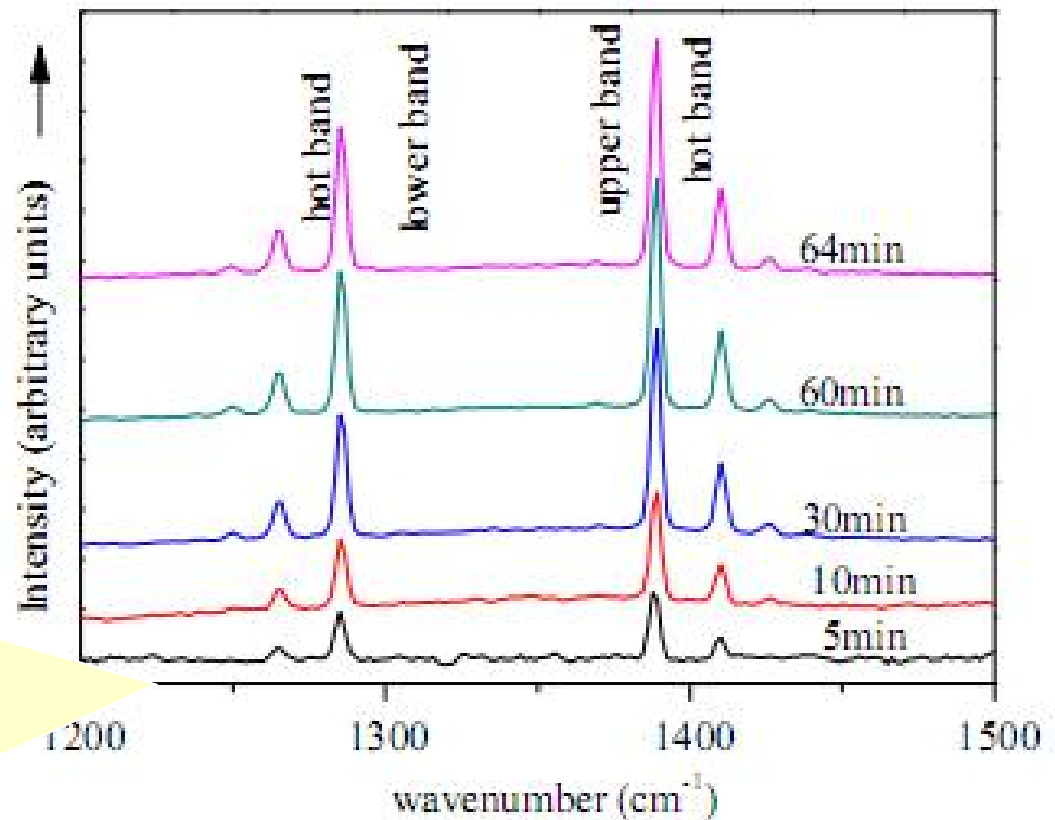
➤ *The Journal of Supercritical Fluids*. 2012, 72:22-27.


























Raman spectra of the vapor phase in FSCR at 260°C collected at different reaction times showing bands for Carbon Tetrachloride (459, 314, and 218  $\text{cm}^{-1}$ ) and product  $\text{CO}_2$  (1286 and 1380

Raman spectra of the vapor phase produced by the hydrolysis of  $\text{CCl}_4$  in HCW at 260°C at various reaction times, showing the  $\text{CO}_2$  bands. and the increase of  $\text{CO}_2$  signals indicates the progress of hydrolysis.



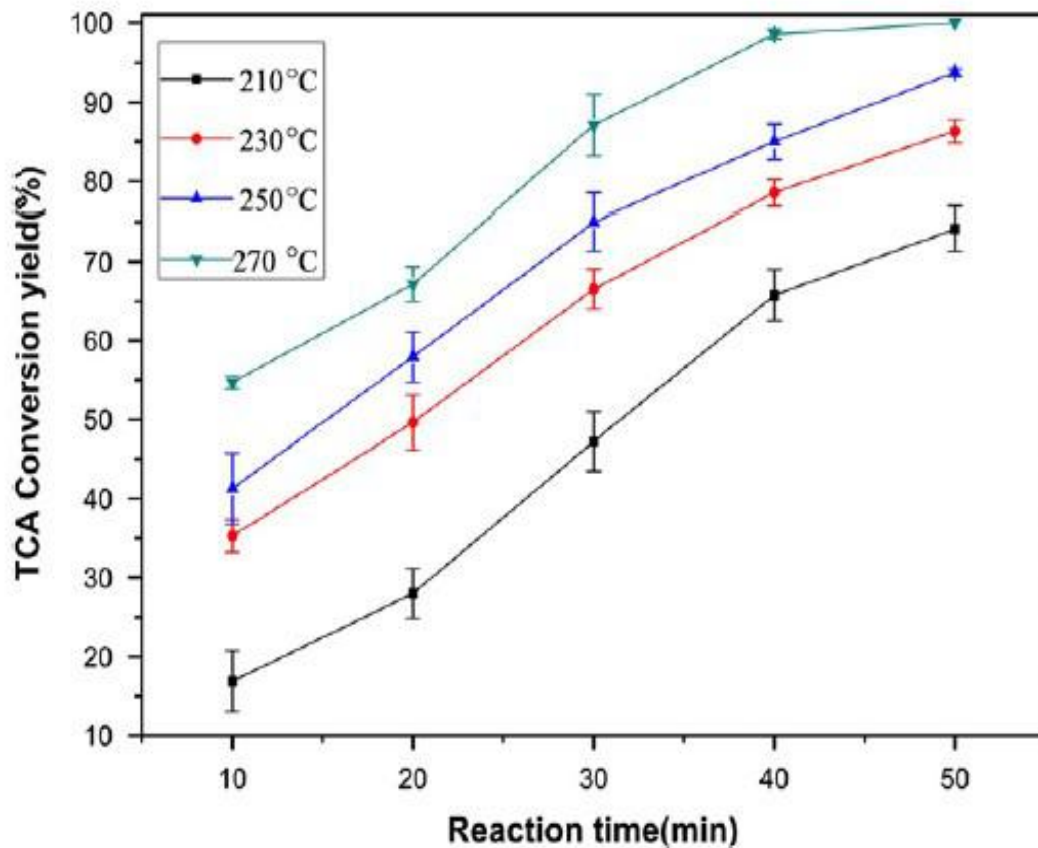
# 3.3 Decomposition of 1,1,1-trichloroethane(TCA) in HCW in FSCR

						
36.5°C	93.3°C	251.7°C	257.2°C	302.9°C	364.4°C	36.1°C
<b>a</b> Heating mixture with deionized water						Cooling
						
30.1°C	92.9°C	144.3°C	252.4°C	369.7°C	400°C	32.1°C
<b>b</b> Heating mixture with excess H <sub>2</sub> O <sub>2</sub>						Cooling
						
31.4°C	93.2°C	144.1°C	226.9°C	369.1°C	400°C	33.2°C
<b>c</b> Heating mixture with insufficient H <sub>2</sub> O <sub>2</sub>						Cooling

shows the hydrolysis of TCA in deionized water during the heating process.

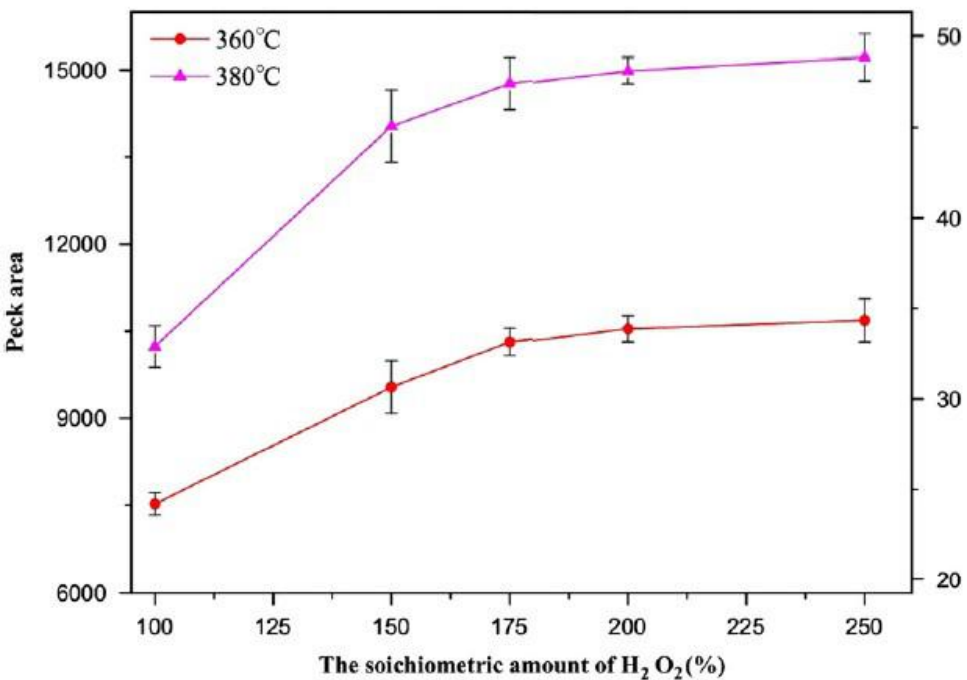
B.P.=74-76

shows the phase behavior during the oxidation of TCA in H<sub>2</sub>O<sub>2</sub> in the heating process.



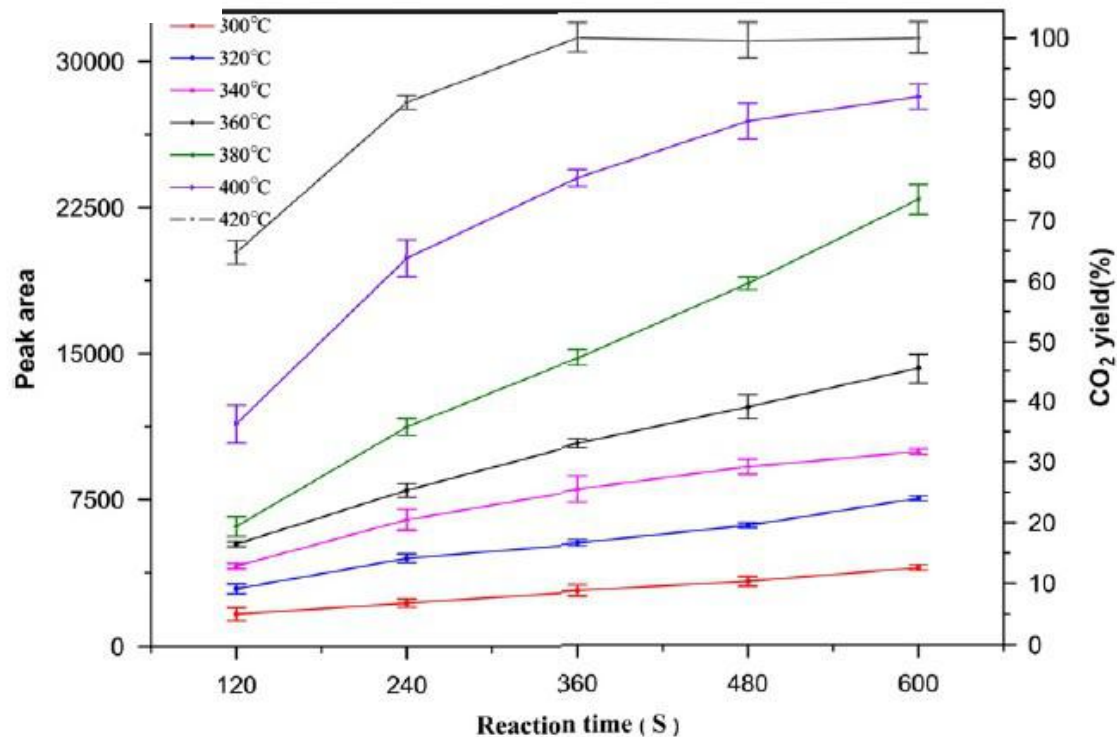
the conversion of TCA increased with increasing temperature in the range 10–50 min, reaching a peak value at 270.°C for 50 min.

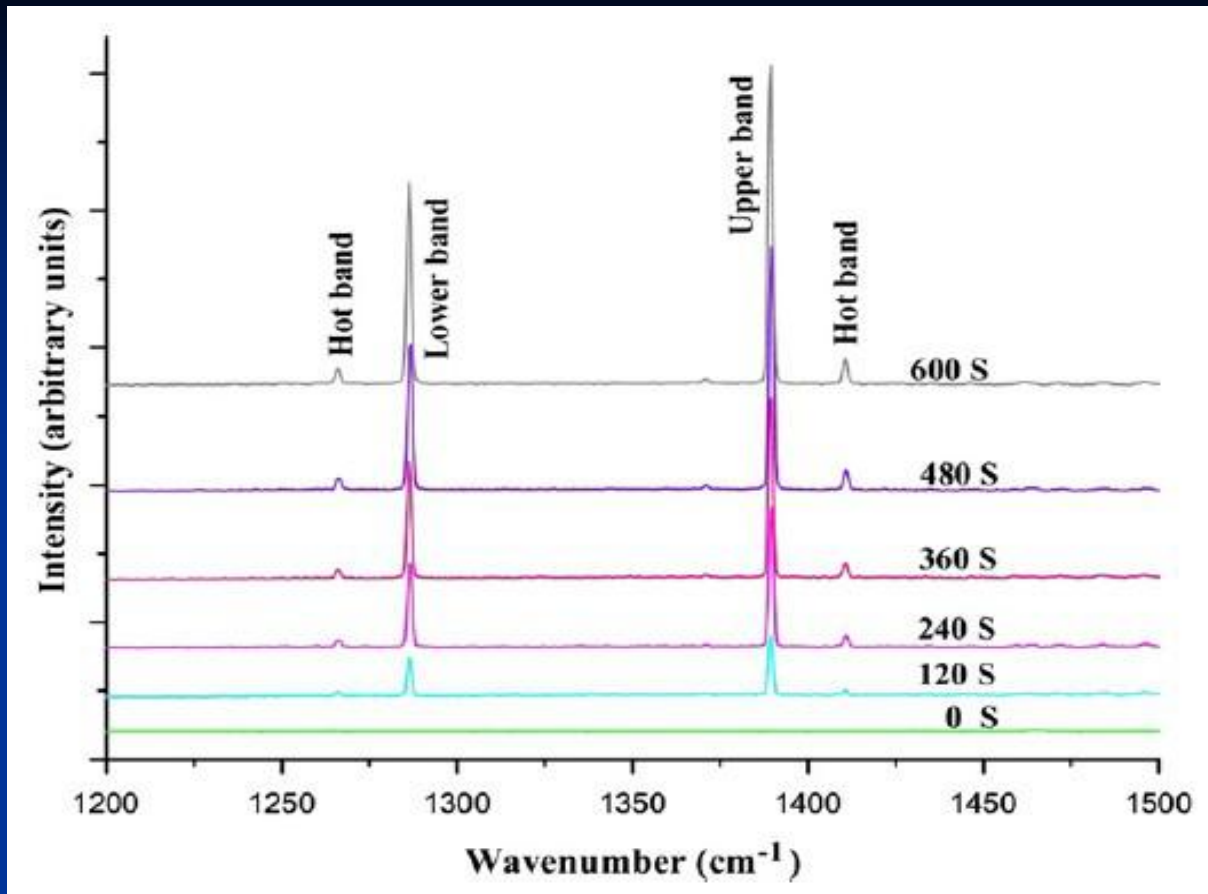
Effect of reaction time on TCA conversion at different temperatures in FSCR.



Effect of stoichiometric amount of H<sub>2</sub>O<sub>2</sub> on Raman peak area of CO<sub>2</sub> yield from TCA (t=6 min).

Raman peak areas of CO<sub>2</sub> and CO<sub>2</sub> yields (lines) with 175% stoichiometric amount of oxidizer at different temperatures and reaction times.





Raman spectra of CO<sub>2</sub> produced by oxidation of TCA in SCWO with 175% stoichiometric amount of oxidizer at 380 °C at different reaction times. The spectra were collected under similar conditions, and the increased CO<sub>2</sub> signals indicate the progress of the oxidation.

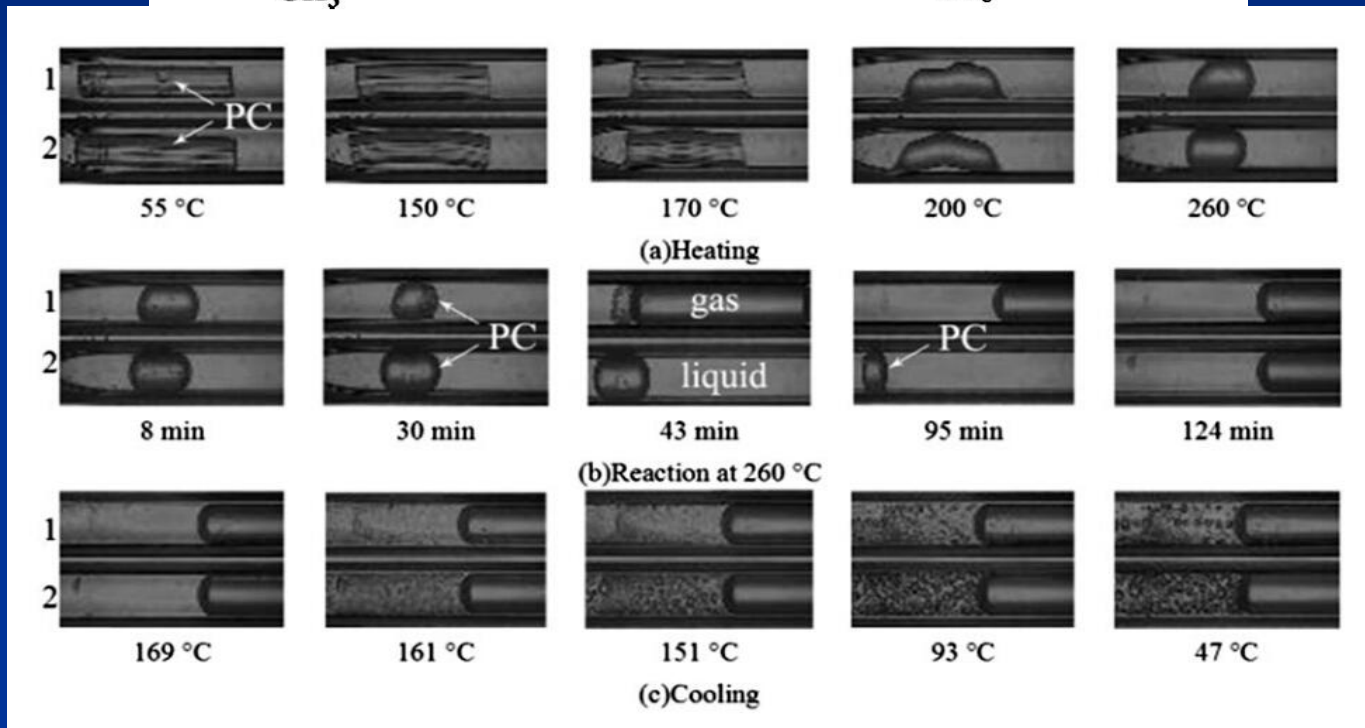
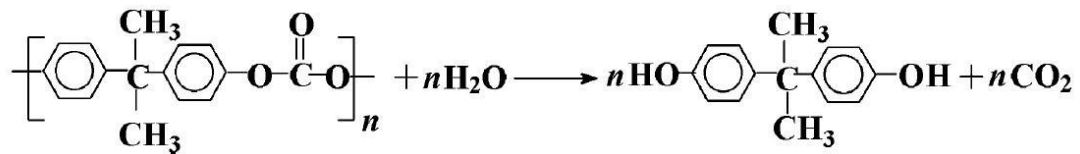
# Depolymerization of polyester in FSCR

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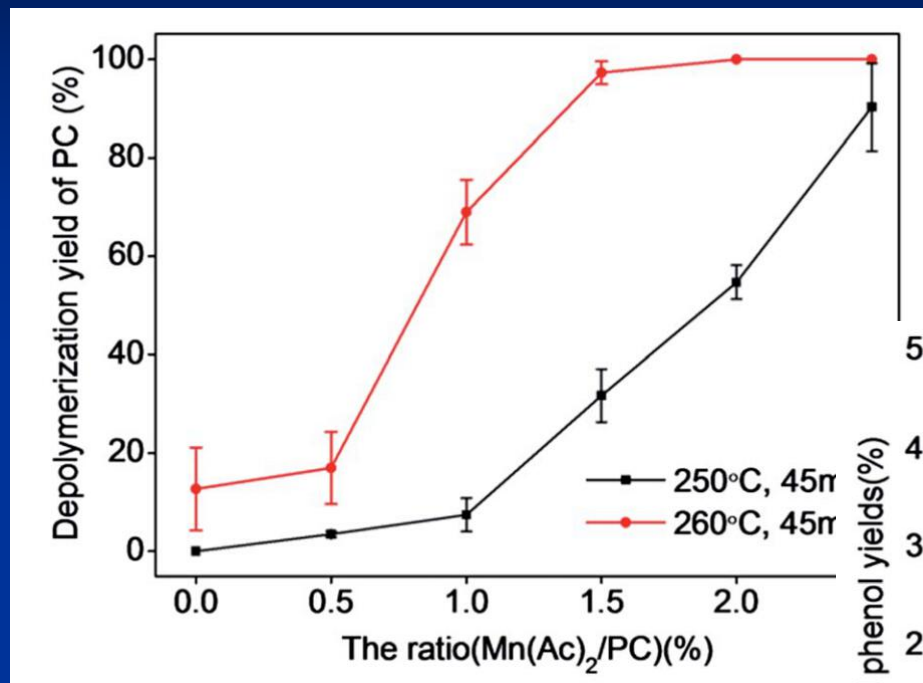
- Depolymerization of PC



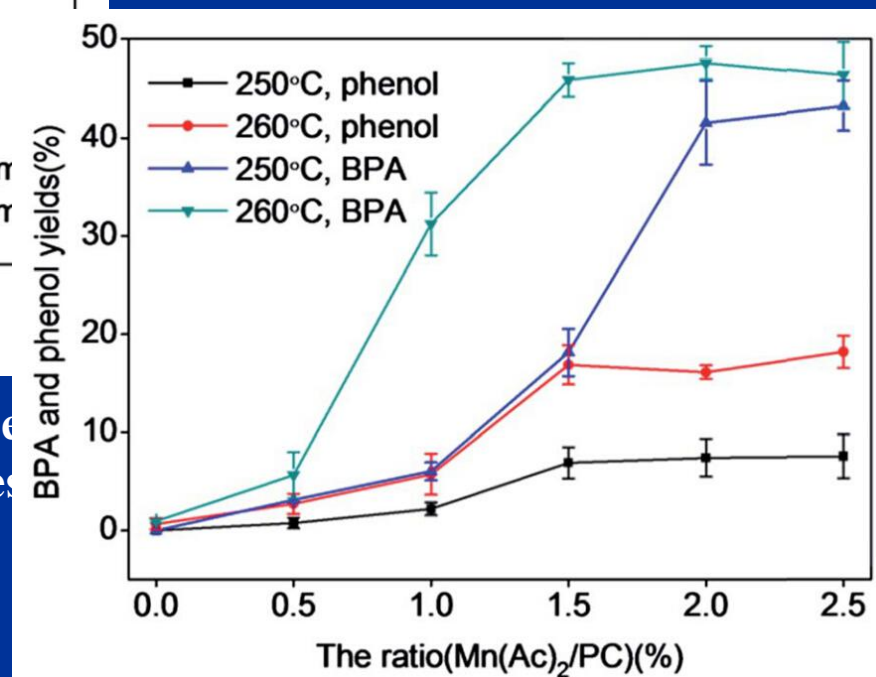
# Depolymerization of polycarbonate(PC)



Photomicrographs of PC in water in FSCR1 and FSCR2. (a) heating process, (b) at different reaction times at 260 C, and (c) cooling process.  $\text{Mn}(\text{Ac})_2$  catalyst was present in FSCR1 and not in FSCR2. The heating/cooling/isothermal schedules were identical for the two FSCRs.

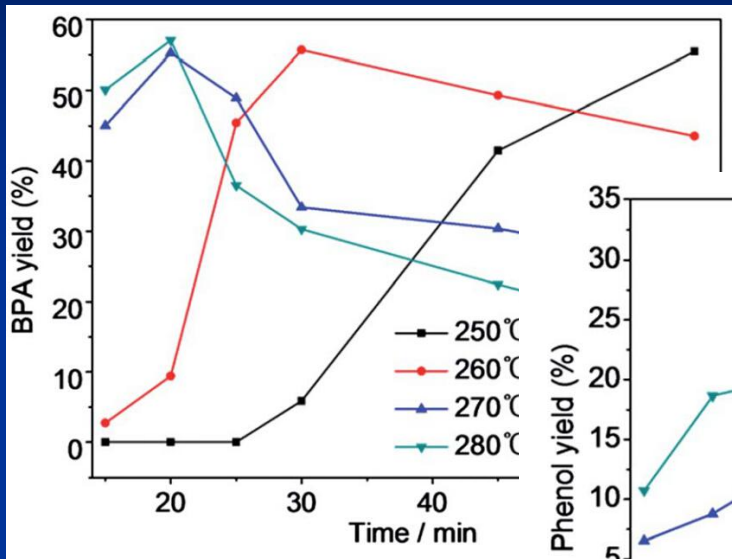


Effect of the  $\text{Mn}(\text{Ac})_2/\text{PC}$  ratio on depolymerization yield of PC at different temperatures

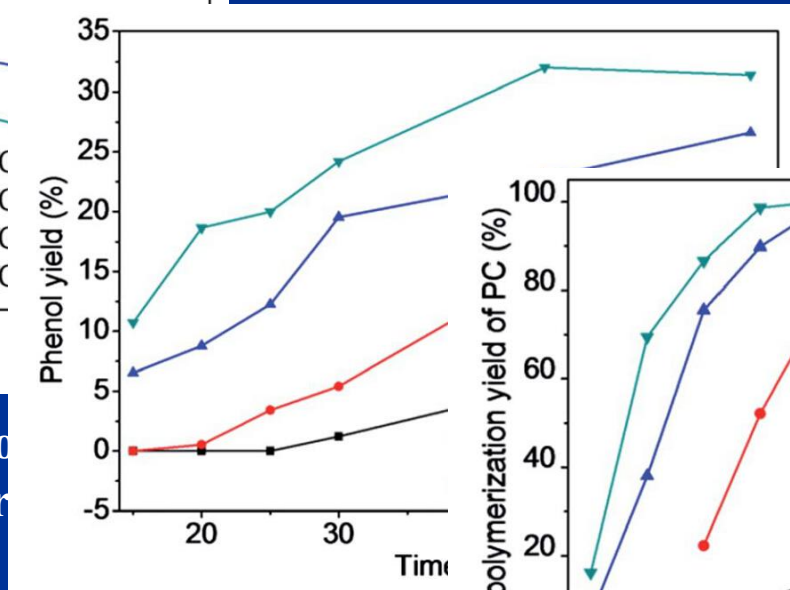


Effect of the  $\text{Mn}(\text{Ac})_2/\text{PC}$  ratio on BPA and phenol yields at different temperatures

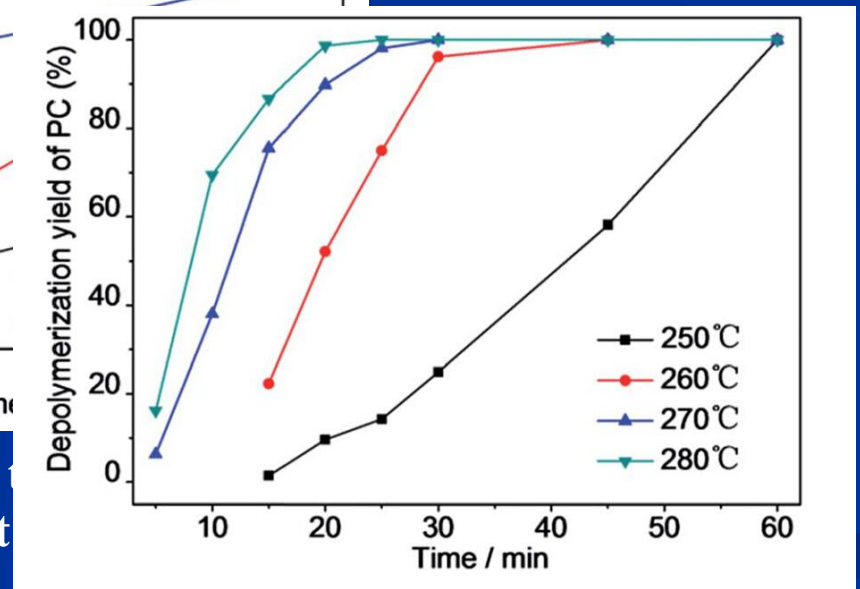




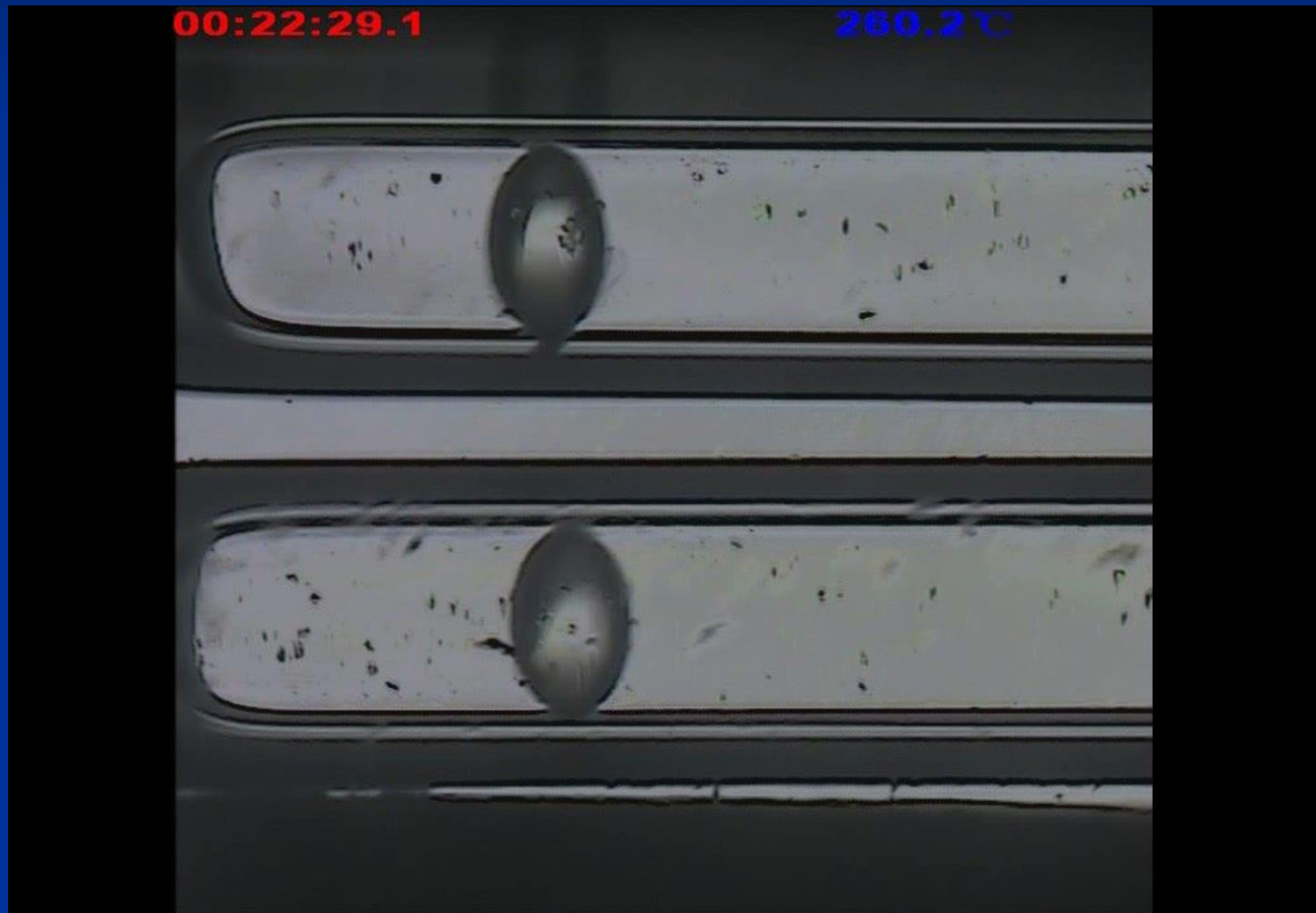
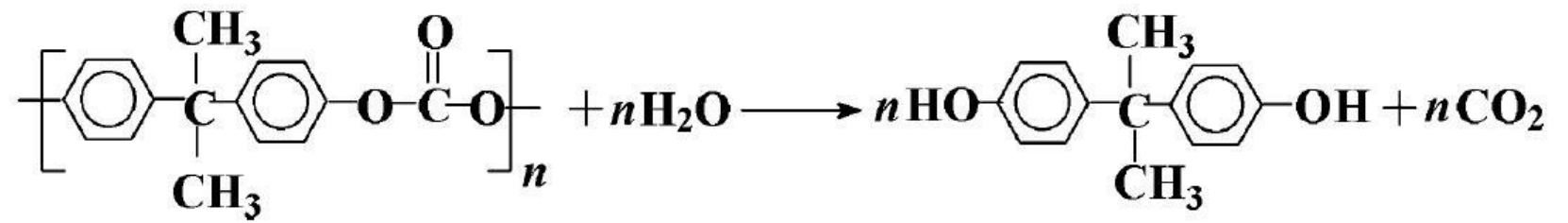
Effect of reaction time on BPA yield at different temperatures



Effect of reaction time on phenol yield at different temperatures



Effect of reaction time on depolymerization yield of PC at different temperatures



# A new method for determining the volume expansion factor of CO<sub>2</sub> + petroleum model compounds



- The traditional methods for expansion
- A new method for determining volume expansion of CO<sub>2</sub> + petroleum model compounds

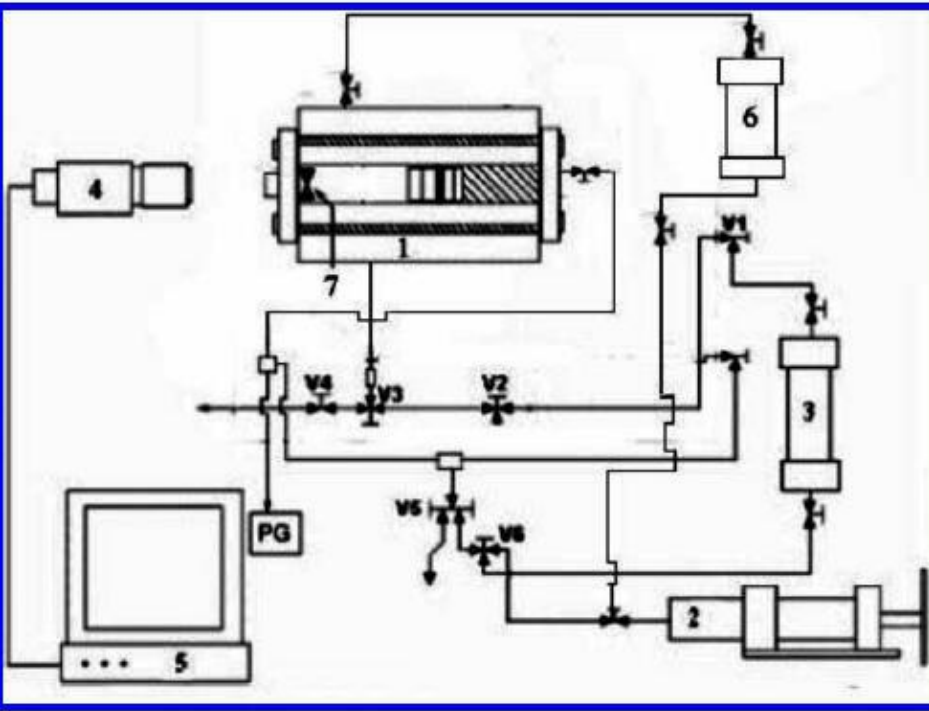
# Enhanced oil recovery(EOR)

- **CO<sub>2</sub> injection has been widely accepted as an effective technique for enhanced oil recovery (EOR) used by the oil industry since 1970s . Injection of CO<sub>2</sub> helps lower the viscosity of crude oil, reduce its interfacial tension, increase its mobility and cause oil swelling in the reservoirs which improves oil recovery. Meanwhile, this technique can effectively reduce greenhouse gas emission by permanent storage of CO<sub>2</sub> in geological formation . As the basic data of CO<sub>2</sub> - EOR, the volume expansion of CO<sub>2</sub> + organic(s) systems have been studied over the past decades with fixed or variable pressure - volume - temperature (PVT) methods.**

# 5.1 The traditional methods for expansion

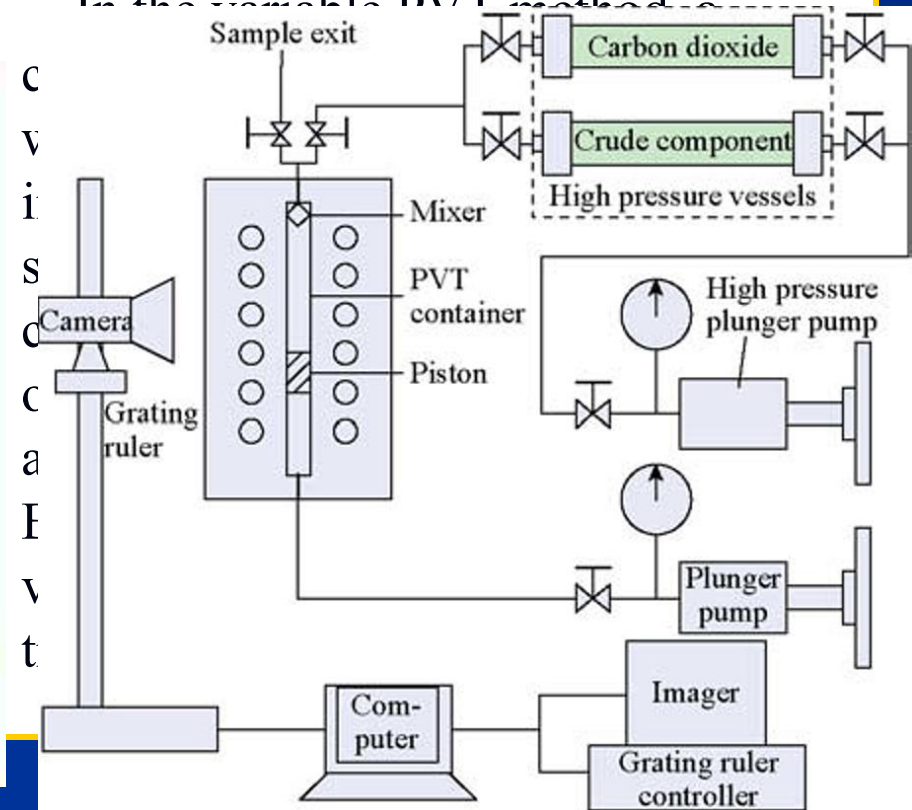
## Fixed PVT method

In the fixed PVT method, certain



## Variable PVT method

In the variable PVT method,





**All of these traditional PVT methods had a high reagents consumption and temperature gradient.**

**The fixed PVT method was easy to cause the vaporization of organic(s) at higher temperatures.**

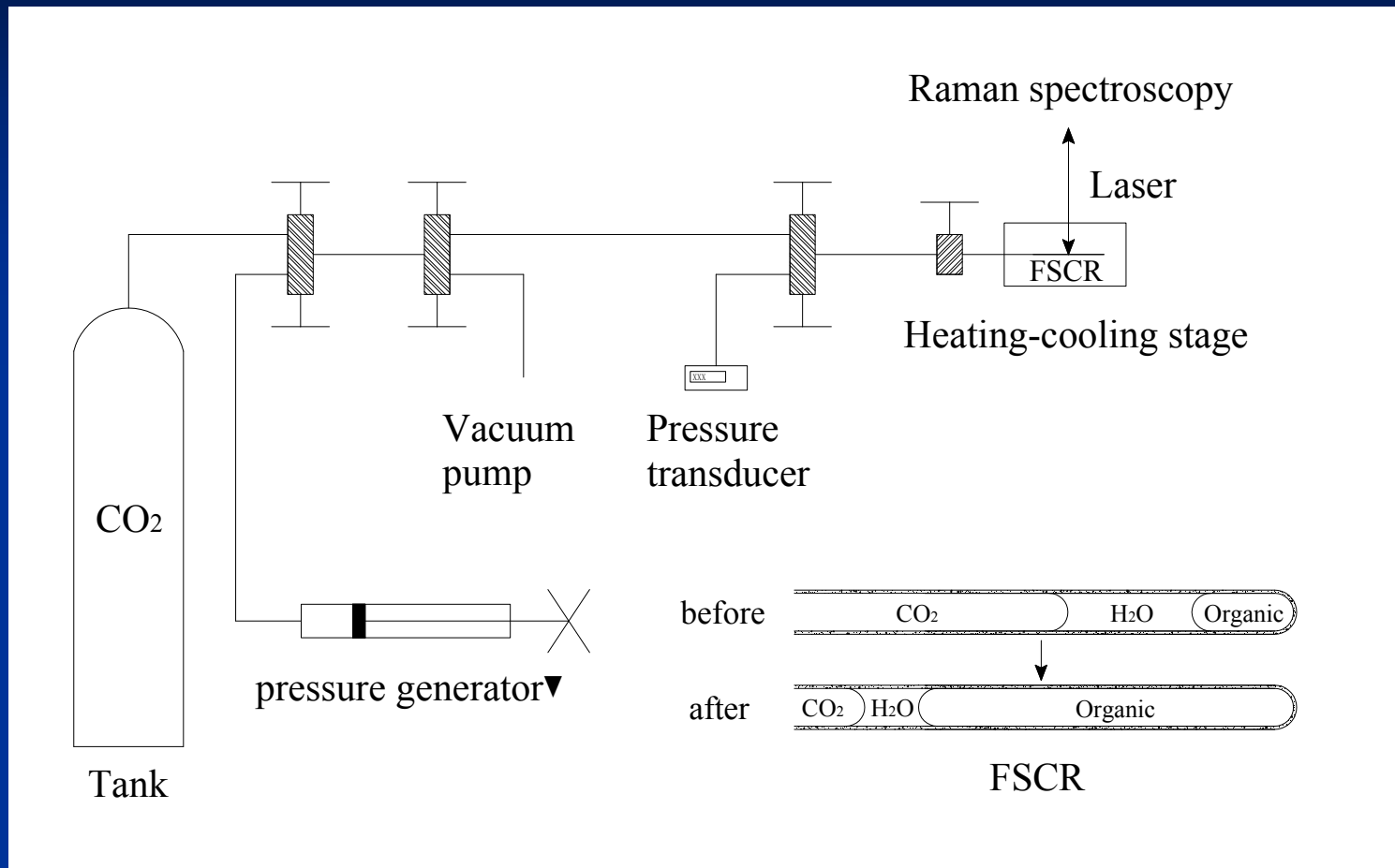
**The variable PVT method was hard to determine the transition point at high CO<sub>2</sub> molar fraction and the CO<sub>2</sub> + organic(s) system was easy to oversaturation at low temperatures.**

## 5.2 A new method for determining volume expansion of CO<sub>2</sub> + petroleum model compounds

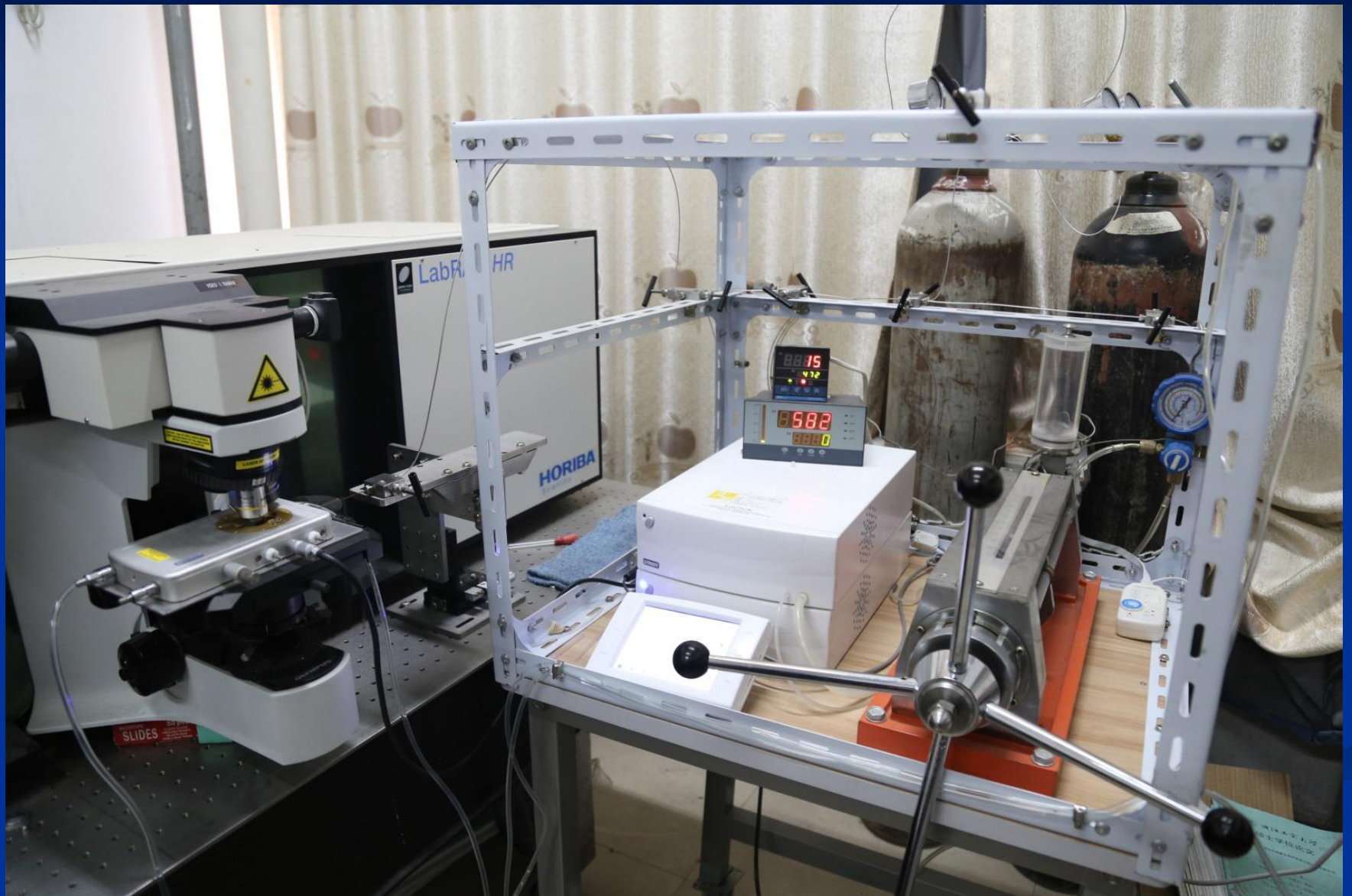
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A new method using a fused silica capillary reactor (FSCR), combined with heating-cooling stage, pressure generator, and co-focal Raman spectrometer has been applied to measuring the volume expansion of CO<sub>2</sub> + petroleum model compounds. **This method using micrometer to measure the volume accurately, water seal to prevent the vaporization of organic(s), a microreactor to decrease the temperature gradient and Raman spectroscopy to ensure system reached phase equilibrium, which is shown to be efficient and generally better than the traditional PVT methods.**





**The schematic diagram of CO<sub>2</sub> + petroleum model compounds volume expansion measuring system.**



# Experimental section A

The procedure for measuring the volume expansion of organic with temperature at atmospheric pressure

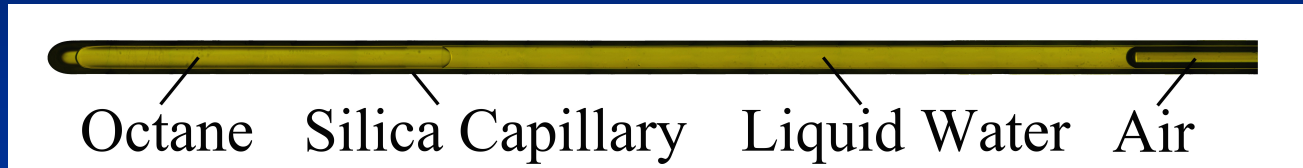
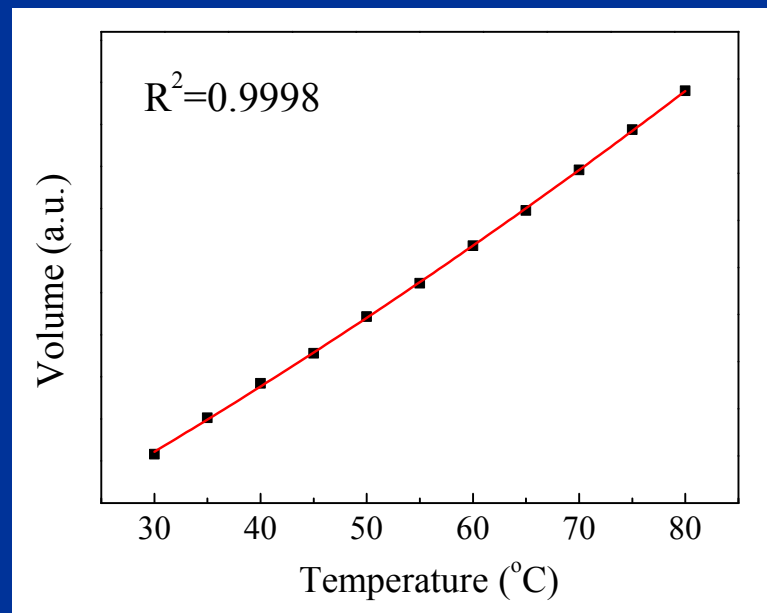


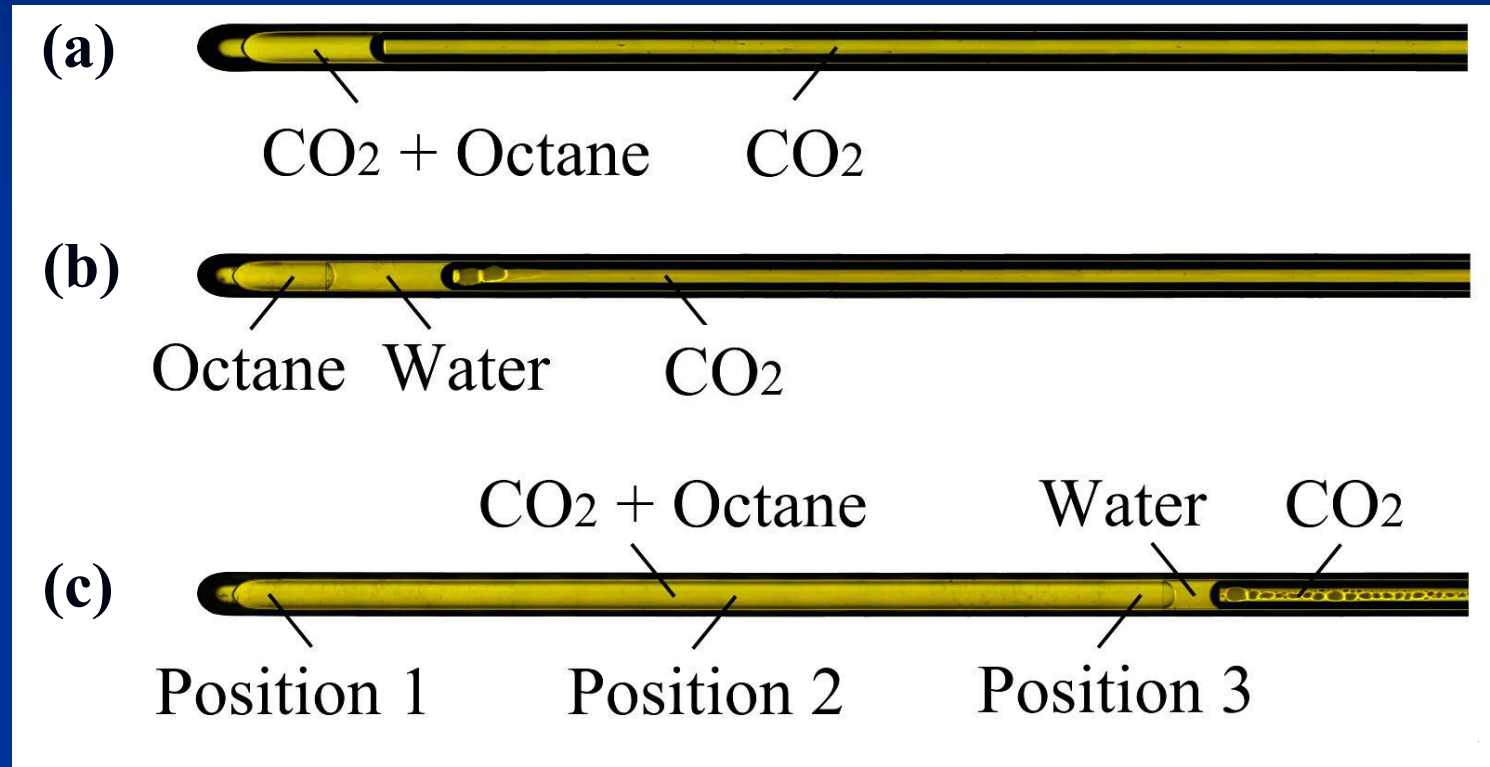
Image of octane in FSCR showing octane, liquid water and air



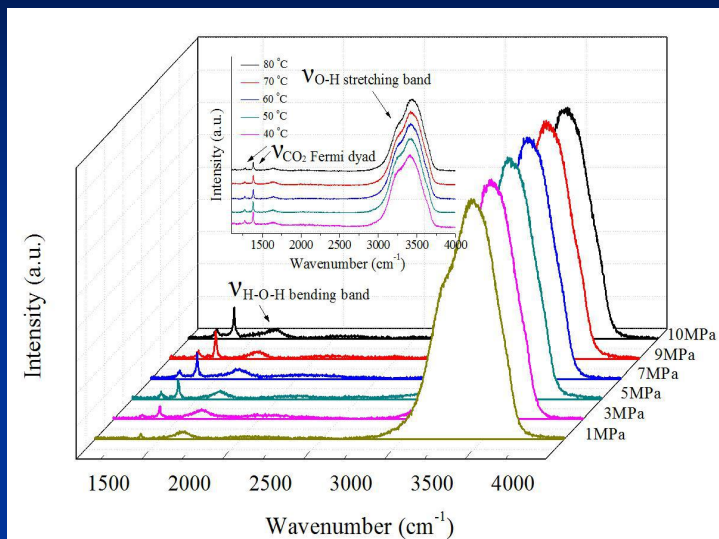
The volume expansion curve of octane from 30 to 80 °C at atmospheric pressure

# Experimental section B

The procedure for measuring the volume expansion of  $\text{CO}_2$  + octane system with temperature at diverse pressure

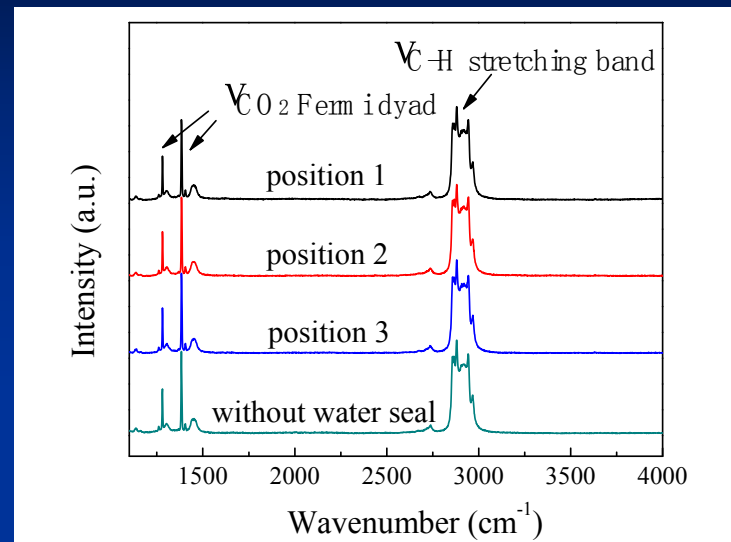


(a) Image of  $\text{CO}_2$  + octane system without water seal in FSCR, showing octane and  $\text{CO}_2$ , (b) Image of  $\text{CO}_2$  + octane system in FSCR before experiment, showing octane, water and  $\text{CO}_2$ , (c) Image of  $\text{CO}_2$  + octane system in FSCR after experiment, positions 1 to 3 indicate the spots for Raman spectroscopy analyses



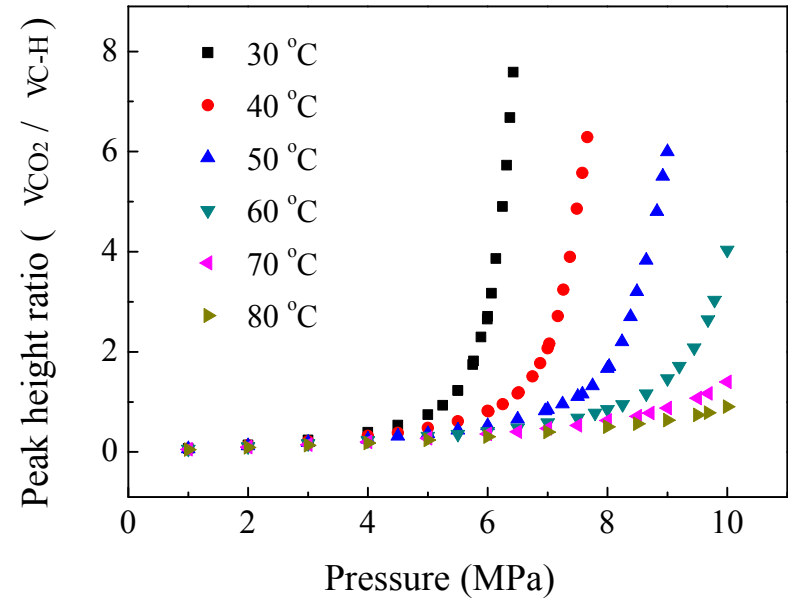
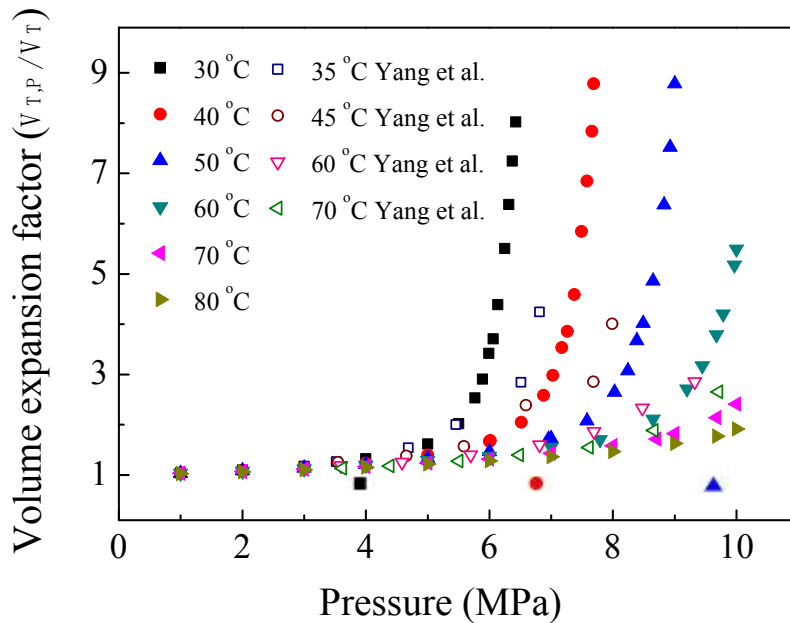
The Raman spectra of water in FSCR from 1 to 10 MPa at 80 °C and from 40 to 80 °C at 8 MPa.

As shown in figure, the Raman spectra of water only contain the H–O–H bending band at  $1629\text{ cm}^{-1}$ , the O–H stretching band in the region of  $2800\text{--}3800\text{ cm}^{-1}$ , and the  $\text{CO}_2$  Fermi dyad at  $1280\text{ cm}^{-1}$  and  $1385\text{ cm}^{-1}$  during the whole procedure, **indicating that octane was not detected in water**



Raman spectra of  $\text{CO}_2$  + octane system at 60 °C, 8 MPa

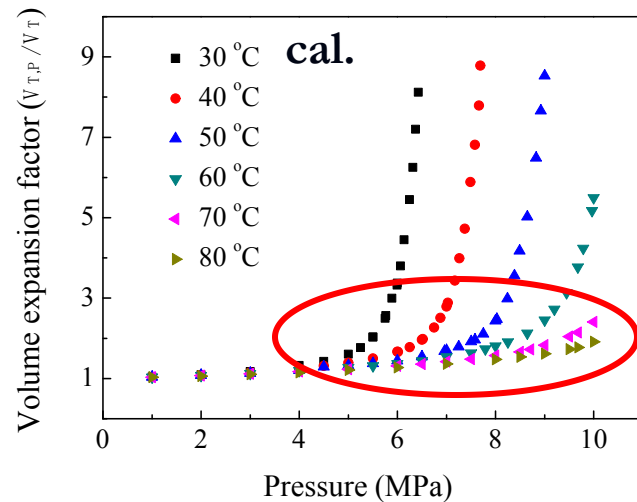
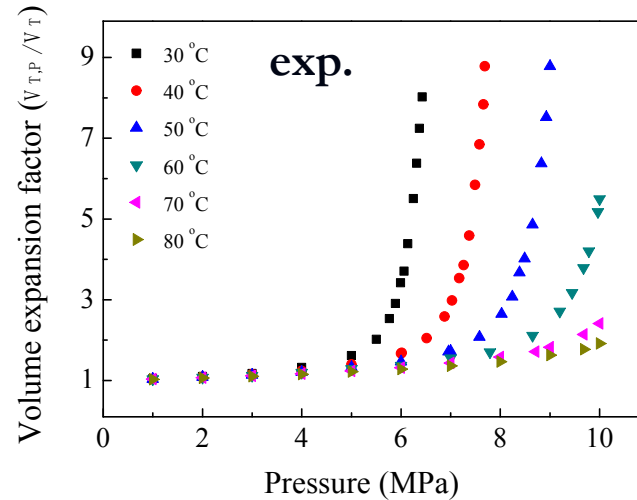
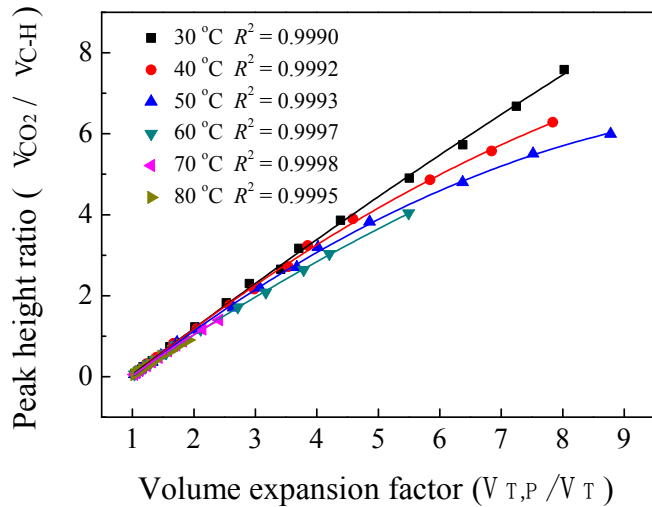
The Raman spectra collected from three different positions in the FSCR showed the same relative band intensities between  $\text{CO}_2$  Fermi dyad and the C–H stretching band of octane at  $1280\text{ cm}^{-1}$ ,  $1385\text{ cm}^{-1}$  and  $2800\text{--}3000\text{ cm}^{-1}$ , **indicating that  $\text{CO}_2$  + octane system reached phase equilibrium becomes a homogeneous solutions in FSCR**



The **volume expansion factor curve** of CO<sub>2</sub> + octane system from 30 to 80 °C and 1 to 10 MPa      The **peak height ratio curve** of CO<sub>2</sub> + octane system from 30 to 80 °C and 1 to 10 MPa

The peak height ratio of CO<sub>2</sub> Fermi dyad and C–H stretching band of octane **had a similar tendency** as the volume expansion factor of CO<sub>2</sub> + octane system



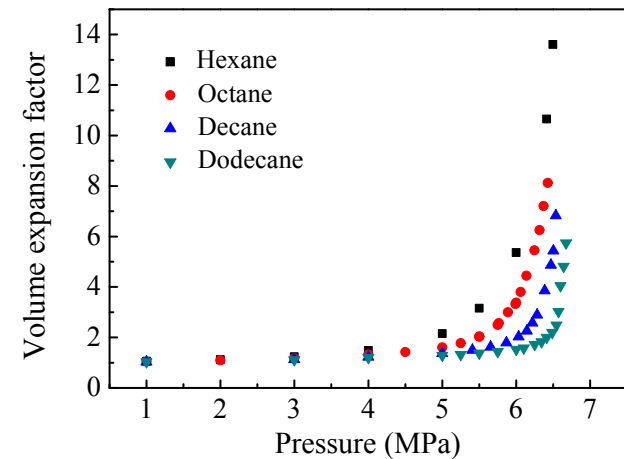


The relationship between the volume expansion factor and peak height ratio of  $\text{CO}_2 + \text{octane}$  system

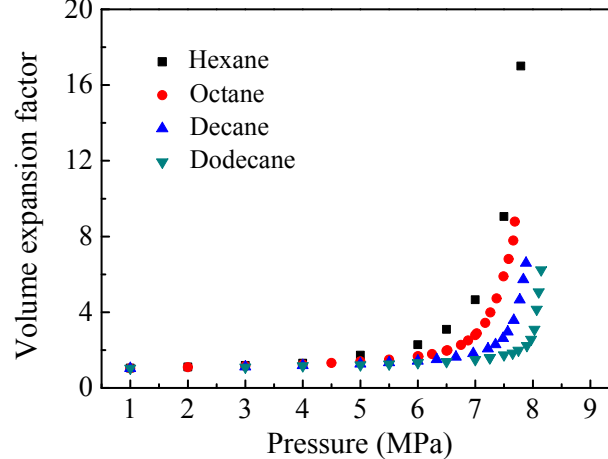
The relationship between volume expansion factor and peak height ratio can be represented by different quadratic equation at different temperature, with  $R^2 \geq 0.999$ . Indicating that **peak height ratio could represent volume expansion factor indirectly.**



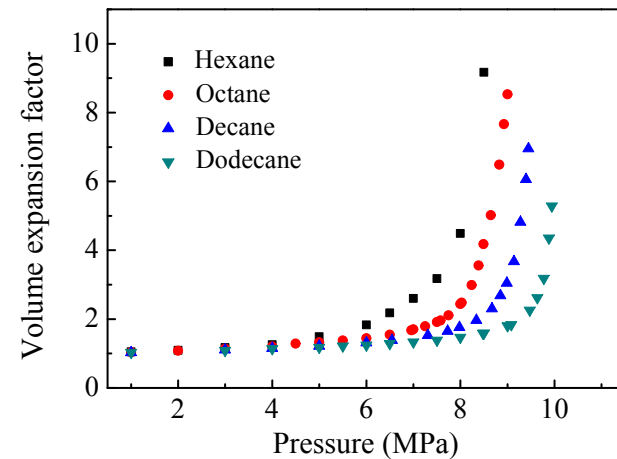
30 °C



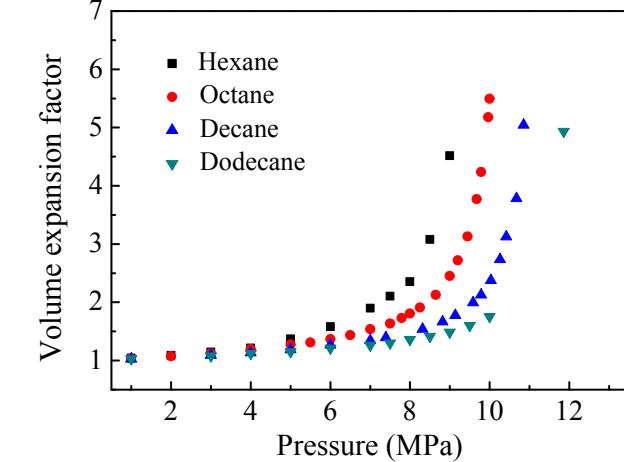
40 °C



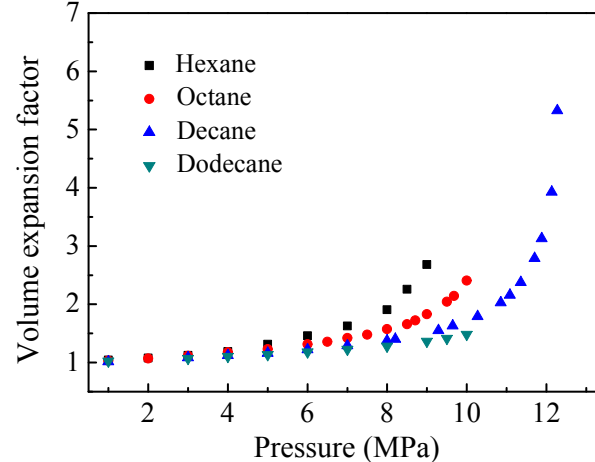
50 °C



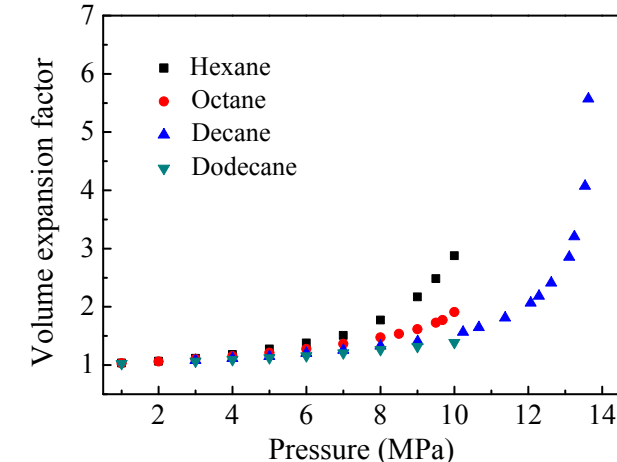
60 °C



70 °C



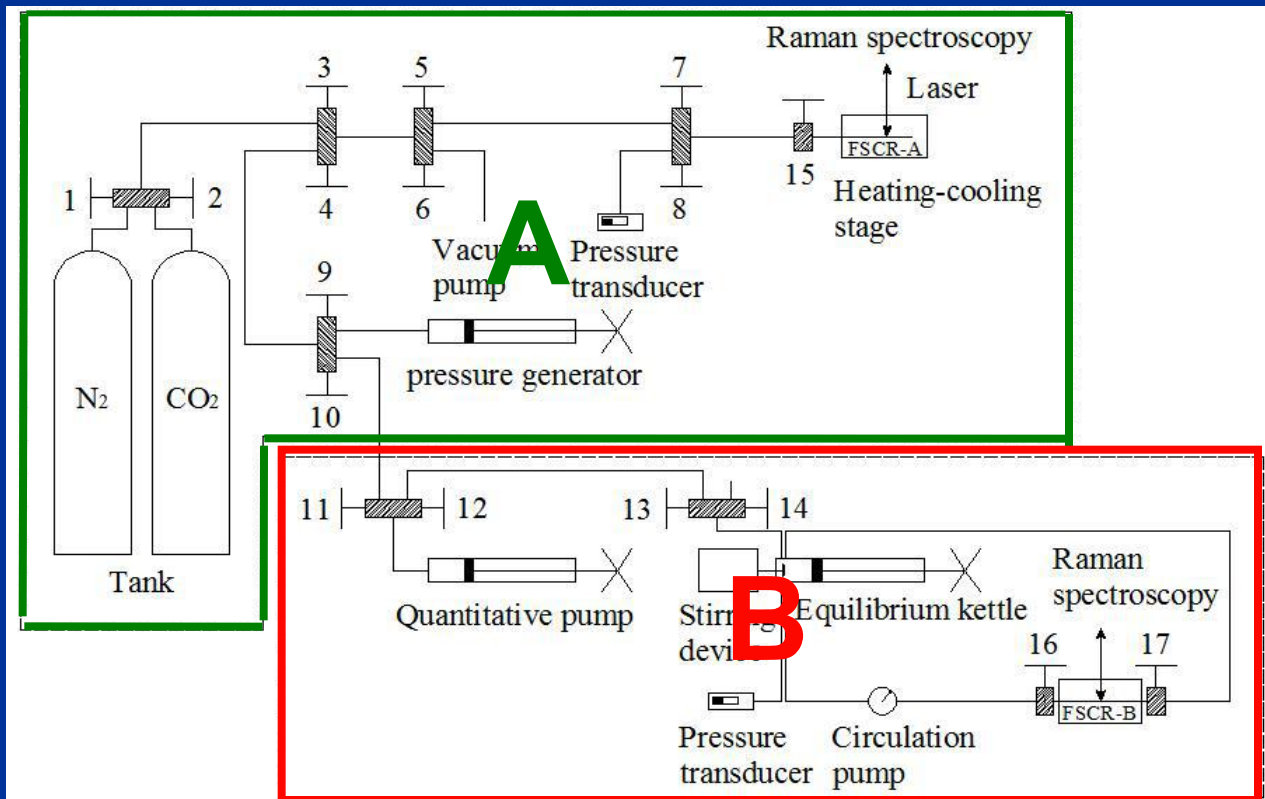
80 °C



The volume expansion factor curve of CO<sub>2</sub> + Hexane/Octane/Decane/Dodecane system

# Future work

A new method using a fused silica capillary reactor (FSCR), combined with heating-cooling stage, pressure generator, equilibrium kettle and Raman spectroscopy has been applied to in-situ measuring CO<sub>2</sub> solubility in brines.



The schematic diagram of CO<sub>2</sub> solubility In-situ determine system





# Summary



- A new method for studying chemical reaction in sub- or super-critical water has been developed.
- Solubility of hydrophobic organic compounds in hot compressed water and SCWO were conducted in FSCR, and in situ Raman spectroscopy was used to analyze the products qualitatively and quantitatively. At the same time, the physical phenomenon was observed under a microscope and the images were recorded by a digital recorder continuously.
- The new method has a great potential for studying chemical reactions in fluids near their critical conditions.



## Advantages of FSCR

- ★ The volume of FSCR is much smaller than that of the stainless autoclave, reducing from milliliter to microlitre:

It is environmental friendly because of the **low amount of material consumed**.

Resistance of mass transfer and heat transfer are reduced, and then the kinetics approach to the **intrinsic kinetics**.

Reactor is **safe** even if explosion happened.

- ★ **Optically transparent** capillary, what happened during reaction can be watched and recorded exactly with the help of microscope and digital recorder, which is much helpful to understand the reaction mechanism by Raman spectra in situ.

- ★ Round-sectioned FSCR with **OD 0.3mm / ID 0.1mm** can withstand **H<sub>2</sub>O** pressures of at least **333 MPa at 600 °C**, and **CO<sub>2</sub>** pressures of at least **350 MPa at 600 °C**, respectively, which can not be done in ordinary reactors easily.

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- [3] Zhiyan Pan, Zhichao Hu, Yinghai Shi, Yuan Shen, Junliang Wang, I-Ming Chou. Depolymerization of polycarbonate with catalyst in hot compressed water in fused silica capillary and autoclave reactors[J]. *RSC Advance*, 2014, 4: 19992-19998.
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THE END

THANKS

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